

ACTIVATED CARBON FROM BAMBOO (*Bambusa vulgaris*) FOR METHYLENE BLUE REMOVAL: PREDICTION TO THE ENVIRONMENT APPLICATIONS

CARVÃO ATIVADO A PARTIR DE BAMBU (*Bambusa vulgaris*) PARA REMOÇÃO DE AZUL DE METILENO: PREDIÇÕES PARA APLICAÇÕES AMBIENTAIS

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ABSTRACT

Activated carbon (AC) is an essential product for the removal of environmental contaminants, but the high production costs limit its use. In this work, AC was produced from bamboo through simultaneous direct physical-chemical activation (by using phosphoric acid and water steam), at 500 °C for 1 hour, to evaluate its adsorption effectiveness for methylene blue dye (MB). Adsorption kinetic and equilibrium studies at batch system were realized at room temperature (to evaluate the adsorption influence of the MB dye over the produced AC) and the Langmuir and Freundlich isotherms systems were selected for understanding the adsorption process. The produced AC showed a relatively high value of surface area equal to 1354.42 m².g⁻¹. The required contact time for the MB to reach equilibrium was 12 hours. The adsorption performance was better delineated by the Langmuir isotherm, which maximum adsorption capacity was of 374.75 mg.g⁻¹. In addition, the R_L dimensionless factor revealed the favorable nature of the adsorption process in the used conditions. The results obtained in this study recommend the use of the produced AC from bamboo in the treatment of the water contaminated by the MB dye, foremost in higher concentrations than limits admitted by the legislation. Finally, complementary researches must be conducted to improve, even more, the quality of the produced material.

Keywords: physical-chemical activation; adsorption; water treatment.

RESUMO

O carvão ativado (CA) é um produto essencial para remoção de contaminantes ambientais, entretanto os altos custos de produção limitam seu uso. Neste trabalho, foi produzido CA a partir de bambu mediante ativação físico-química simultânea direta (utilizando ácido fosfórico e vapor d'água), a 500 °C por 1 hora, para avaliar sua eficácia na adsorção do corante azul de metileno (AM). Estudos cinéticos e de equilíbrio de adsorção em sistema batelada foram realizados em temperatura ambiente (para avaliar a influência da adsorção do corante AM sobre o CA produzido) e os modelos de isotermas de Langmuir e de Freundlich foram selecionados para entender o processo de adsorção. O CA produzido apresentou um valor relativamente alto de área superficial igual a 1354,42 m² g⁻¹. O tempo de contato preciso para o AM atingir o equilíbrio foi de 12 horas. O desempenho da adsorção foi melhor delineado pelo modelo dado pela isoterma de Langmuir, cuja capacidade máxima de adsorção foi de 374,75 mg g⁻¹. E o fator adimensional R_L revelou a natureza favorável do processo de adsorção nas condições realizadas. Os resultados obtidos neste estudo

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recomendam o uso do CA produzido a partir de bambu no tratamento de água contaminada pelo corante AM, mormente em concentrações maiores que os limites permitidos pela legislação. Finalmente, pesquisas complementares devem ser realizadas para aprimorar, ainda mais, a qualidade do material produzido.

Palavras-chave: ativação físico-química; adsorção; tratamento de água.

INTRODUCTION

According to the United Nations, in 2030 half of the world's population will live in water shortage areas (NAÇÕES UNIDAS, 2016), a situation already experienced in several countries in the world. That account presages the diversified search for new technologies that allows the decontamination/reuse of the water, aiming, for example, for the dye removal from water bodies.

Alluding to the dyes, these correspond to a multiplicity of organic compound introduced in the water, especially through wastes of textile, paper, pharmaceutical and tannery factories, which causes significant problems to the environment, such as the increase of toxicity and lower oxygen demand, besides the light penetration reduction in some environments, which acts in the photosynthetic phenomena (BULUT; AYDIN, 2006; CARMEN; DANIELA, 2012; MEZOHEGYI et al., 2012).

That been said, adsorption Kinetic and equilibrium studies are being executed in search for comprehending the dyes adsorption mechanisms. Among them, the methylene blue stands out, which lies as an extensively researched and studied dye in adsorption on solids, repeatedly presented as a model compound to be followed in adsorption studies of organic compounds from aqueous solutions (HAMEED; DIN; AHMAD, 2007; AVELAR et al., 2010; COUTO et al., 2012; BORGES et al., 2016).

In this scenario, the activated carbon appears as a very promising technology for the dye removal from an aqueous solution (AVELAR et al., 2010; PEZOTI JR et al., 2016). A promising technology because, in theory, nowadays, the activated carbon is one of the main adsorbents researched for the removal of contaminants in the water (NJOKU; FOO; HAMEED, 2013; NJOKU et al., 2014).

Even not being the only adsorbent in this intent, search for this product has wildly increased for its high surface area, which facilitates the adsorption capacity, mainly when used for separating contaminants in a purification process, having an important part in chemical, pharmaceutical and food industries, which makes an increasing coverage breadth of this product in the world consumption (HAYASHI et al., 2002; AVELAR et al., 2010; ROMERO-ANAYA et al., 2014; CESKAA, 2016), because of the increase of the pollution levels, health problems and increasing governmental regulations that claims for anti-pollution alternatives (CESKAA, 2016).

The search and necessity of this material is reflected on the global market, with the AC in 2015 being evaluated in 2.7 billion dollars, boosted mainly by the USA and the Asia-Pacific region. There are talks of the probability of this value to reach 5.1 billion dollars until 2021 (CESKAA, 2016).

As a profusely porous material, the activated carbon is originated from the activation process, that involves the thermic and/or chemical treatment of the raw material, that, in the present study, is the bamboo, although the lack of vast raw materials in this regard conducted the researchers to find less costly new precursors for AC preparation (HAMEED; DIN; AHMAD, 2007; HAMEED; EL-KHAIARY, 2008; AVELAR et al., 2010; COUTO et al., 2012; NJOKU; FOO; HAMEED, 2013; BARBOSA et al., 2014; BORGES et al., 2016; LINHARES; MARCÍLIO; MELO, 2016; PEZOTI JR et al., 2016).

In the AC production process physical or chemical activating agents are used, being responsible for promoting the porosity increase and thus the surface area increase. The main activating agents used on the AC production are water steam, carbon dioxide, zinc chloride, and phosphoric acid. About the activation processes, two are applied: the physical or chemical activation. The physical activation is the one that revolves around the synthesis of the raw material at elevated temperatures that varies from 700 to 1000 °C and the use of a physical activating agent such as water steam or carbon dioxide; while the chemical activating covers the synthesis of the raw material at lower temperatures that varies from 400 to 700 °C in which, in a previous step of the thermal treatment, the raw material is impregnated with a concentrated solution of an activating agent such as zinc chloride and phosphoric acid. Nowadays, both of the process can be used concomitantly.

Next to this, there are the connected variables of the AC production process as activation temperature, residence time and proportion of the used activating agent proportion must be considered, because they have influence over the final processing costs and becoming a competitive differential. Therefore, when the process variables are enhanced and the quality is assured, the production costs are reduced.

According to the stated, in order to contribute to the enhancement of AC that can be used to water treatment, this article discusses the production of these materials, that have the bamboo as raw material, and analyses the results of their applications from kinetic and adsorption equilibrium studies for the MB dye.

MATERIAL AND METHODS

Activated carbon production and BET surface area

The specie herein used, *Bambusa vulgaris*, came from two-year-old plantations from the Celulose e Papel de Pernambuco S.A. (CEPASA) of the Grupo Industrial João Santos, located in Jaboatão dos Guararapes, Pernambuco state, Brazil. The raw material was impregnated with a H_3PO_4 concentration solution at 2:1 (m:m), under agitation at 80 °C in a magnetic shaker (Fisatom, São Paulo, Brasil) for 2h. Then, it was dried at a conventional oven at 103 ± 2 °C for 24h and thereon activated at a CHINO rotating electric oven (Takabayashi Rica, RS-S model, Japan), containing a tubular reactor (93 mm internal diameter and 900 mm length), an electric boiler and an attached dewar container with N_2 .

The activation process was made effective at a final temperature of 500 °C, with a $10\text{ °C}.\text{min}^{-1}$ heating rate, residence time of 1 hour with water steam flux of $100\text{ mL}.\text{min}^{-1}$ and N_2 flux of $80\text{ mL}.\text{min}^{-1}$. When the process ended, the oven was turned off, the N_2 flux maintained until 300 °C and the AC taken off the oven after 150 °C (Figure 1). The obtained AC, called $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC, was washed with distilled water, alternately hot and cold, until neutral pH. After the washing, it was dried at kiln at 103 ± 2 °C for 24h.

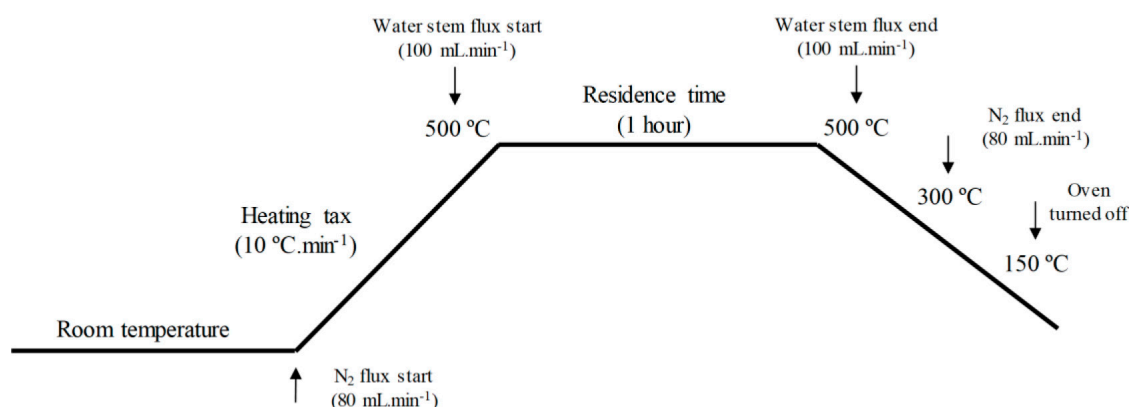


FIGURE 1: Heating ramp used in the activation process.

FIGURA 1: Rampa de aquecimento utilizada no processo de ativação.

The BET surface area was made with the gaseous step adsorption data obtained using an automatic adsorption system (Autosorb-6, Quantachrome Corporation, USA), after the sample was vacuum-degasified at 250 °C. The method employs the nitrogen (N₂) adsorption technique at 77 K and is based on the BET - Brunauer, Emmett and Teller (SKAAR, 1988; MEDEIROS, 2008) works, as represented in Eq. (1).

$$V_a = \frac{V_m \times C \times P}{(P_0 - P) \left[1 + (C - 1) \left(\frac{P}{P_0} \right) \right]} \quad (1)$$

where: V_a = adsorbed gas amount at P pressure (mL); V_m = adsorbed gas amount when all surface is covered by a monomolecular layer (mL); C = Surface interaction energy constant and P_0 = gas saturation pressure.

Evaluations for applications of the studied activated carbon and adsorbate

Aiming to evaluate the H₃PO₄/H₂O AC use in the water treatment, adsorption studies were made with the amorphous natured cationic dye methylene blue, produced by Proquimios Comércio e Indústria Ltda. (Rio de Janeiro, Brazil), with 319.85 g.mol⁻¹ molar mass (Figure 2). All the solutions were prepared with distilled water and obtained by dilution of the initial solution of MB with a 1000 mg.L⁻¹ concentration.

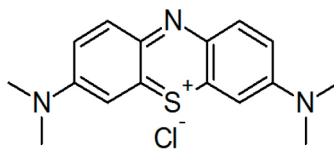


FIGURE 2: Chemical structure of methylene blue (MB).

FIGURA 2: Estrutura química do azul de metileno (AM).

Effect of the contact time

The effect of the adsorbate/adsorbent contact time was obtained by using 10 mg of H₃PO₄/H₂O AC and 10 mL of methylene blue solutions at a 50 mg.L⁻¹ concentration, which were put in a set of 20 mL containers that were sealed shut and then kept under rotation in a shaker (SL 221, SOLAB, São Paulo, Brazil), with a 100 rpm rotation control and room temperature (the analysis was made in duplicate and an average value of the results were taken).

At predetermined intervals of 1, 3, 6, 12 and 24h, aliquots of the solutions were taken and their concentrations determined by using the characteristic wavelength (λ) of the MB dye, $\lambda = 665$ nm. The UV-VIS spectrophotometer (Shimadzu, UV-mini 1240, Japan) were used to determine the dye concentrations. The MB amount that was adsorbed in a t, q, (mg.g⁻¹) time was calculated according to the Eq. (2).

$$q_t = \frac{(C_0 - C_t) \times V}{m} \quad (2)$$

where: C_0 and C_t = represent, respectively, the dye concentrations at liquid phase, initial and in the predetermined time intervals (mg.L⁻¹); V = adsorbate volume (L); and m = adsorbent mass (g).

Adsorption isotherm

For this essay, the same initial procedures described for the adsorption kinetic study were made, providing that the 20 mL container set were kept under rotation in a shaker for 24h, at room temperature, until they reach the adsorption equilibrium. After this period, they were removed from the shaker, the samples were filtered and the equilibrium concentration determined in the UV-VIS spectrophotometer, in absorbance punctual analysis ($\lambda = 665$ nm). Calibration curve were made with methylene blue solutions at 25, 50, 100, 250, 500 and 1000 mg.L⁻¹ concentrations. The adsorbed adsorbate (methylene blue) amount per adsorbent gram (H₃PO₄/H₂O AC), q_{eq} (mg.g⁻¹), was calculated according to the Eq. (3).

$$q_{eq} = \frac{(C_0 - C_{eq}) \times V}{m} \quad (3)$$

where: C_0 and C_{eq} = represent, respectively, the initial and at balance concentrations (mg.L⁻¹); V = the adsorbate volume (L) and m = the adsorbent mass (g).

RESULTS AND DISCUSSION

BET surface area

The obtained H₃PO₄/H₂O AC presented BET surface area (S_{BET}) equal to 1354.42 m².g⁻¹, which compares to other adsorbents found in literature as show in Table 1.

TABLE 1: Surface area (S_{BET}) obtained for various adsorbents.

TABELA 1: Área superficial (S_{BET}) obtida para vários adsorventes.

Raw material	Used processes		S_{BET} (m ² .g ⁻¹)	Reference
	Carbonization	Activation		
Bamboo	-	H ₃ PO ₄ /H ₂ O, 500 °C, 1h	1354.42	This work
Bamboo	700 °C, 1h	KOH/CO ₂ , 850 °C, 2h	1896.00	Hameed et al. (2007)
Bamboo	500 °C, 1h	K ₂ CO ₃ /CO ₂ , 850 °C, 2h	1724.00	Hameed and El-Khaiary (2008)
Bamboo	-	H ₃ PO ₄ /H ₂ O, 500 °C, 1h	1196.30	Santana et al. (2017)
Piassava	-	ZnCl ₂ , 500 °C, 3h	1190.00	Avelar et al. (2010)
<i>Eucalyptus</i> sp.	800 °C, 4h	CO ₂ , 800 °C, 4h	1034.07	Grima-Olmedo et al. (2016)
Black wattle	-	H ₃ PO ₄ , 500 °C, 2h	905.68	Linhares et al. (2016)
Piassava	-	H ₃ PO ₄ , 500 °C, 3h	747.00	Avelar et al. (2010)
Rubber tree	-	H ₃ PO ₄ , 800 °C, 4h	693.00	Thubsuang et al. (2017)
Water hyacinth	-	ZnCl ₂ , 700 °C, 1h	640.00	Barbosa et al. (2014)
<i>Eucalyptus</i> sp.	-	K ₂ CO ₃ , 500 °C, 3h	539.00	Couto et al. (2012)
Carnauba palm	-	CaCl ₂ , 500 °C, 1h	430.69	Lacerda et al. (2015)
Stone pine	-	H ₃ PO ₄ , 500 °C, 1h	296.01	Lacerda et al. (2015)

It can be noted that the H₃PO₄/H₂O AC presented a relatively high surface area when compared to the S_{BET} values in the literature, which varies from 296.01 to 1896.00 m².g⁻¹. This performance has great

influence in the adsorption because, usually, a greater surface area mean elevated contaminant adsorption capacity, with the S_{BET} as an important aspect to be used for selecting the adsorbents (activated carbon) in contaminant separation processes (BARBOSA et al., 2014).

The $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC S_{BET} was inferior to the ones obtained by the bamboo in the works of Hameed, Din and Ahmad (2007) and Hameed and El-Khaiary (2008). That happened because of the changes in the AC production process in this work, which used a direct simultaneous physicochemical activation process, where the carbonization and activation stages occurred simultaneously, possibly resulting in lower production costs for AC and keeping a $S_{\text{BET}} > 1000 \text{ m}^2.\text{g}^{-1}$.

It has to be said that the development of the porous structure of the AC depends on the used activation process (ABBAS; KADDOUR; TRARI, 2014) and that the simultaneous activation promotes a higher increment in pores and consequently in surface area (HAMEED; EL-KHAIARY, 2008), as observed.

Also, the higher the residence time, and activation temperature employed in the process, more elevated will be the AC production costs and the possible damage to the oven. In this scenario, trying to reduce the costs, the residence time (1h) and activation temperature (500°C) used were lower than the literature. Studies on the residence time and activation temperature are extremely important in the energetic viability because higher temperatures demands a higher energy cost and, depending on the objective for the application of the material, the activation can become unfeasible (BORGES et al., 2016).

When we relate the obtained S_{BET} in this study with the established improvements in the process, it can be concluded that the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC is an adsorbent that can be obtained certainly at a low cost.

Effect of the contact time

This experiment was made intending to evaluate the effect of the initial methylene blue concentration ($C_0 = 50 \text{ mg.L}^{-1}$) due to the adsorbate/adsorbent contact time at room temperature. A vertiginous dye adsorption was observed until the 6h time interval and after this period a milder adsorption. The necessary time to reach the adsorption equilibrium was 12h ($q_t = 49.85 \text{ mg.g}^{-1}$) and the adsorbed dye amount, q_t , was elevated within the adsorbate/adsorbent contact time. Within 24h of reaction, the AC had absorbed almost all the dye present in the initial solution (Figure 3).

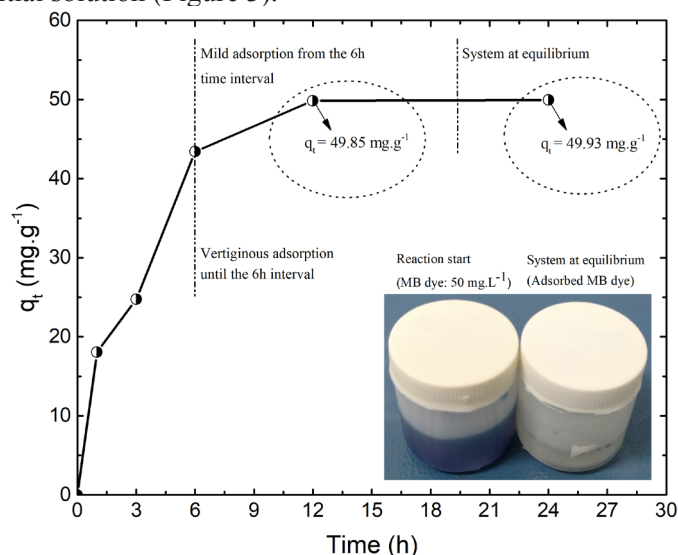


FIGURE 3: Effect of contact time on the initial MB dye concentration (10 mg AC; 10 mL 50 mg.L^{-1} solution; q_t = amount of adsorbed dye in a t time; at room temperature).

FIGURA 3: Efeito do tempo de contato sobre a concentração inicial do corante AM (10 mg de CA; 10 mL de solução 50 mg.L^{-1} ; q_t = quantidade de corante adsorvido no tempo t; em temperatura ambiente).

A great number of the AC active site were empty in the initial adsorption stages, resulting in a faster adsorption. Within time, the competition for the AC active sites is softened, delaying the adsorption (ISLAM et al., 2015). The percentage of MB dye removal, $R(\%)$, was obtained according to Eq. (4).

$$R(\%)_t = \frac{(C_0 - C_t)}{C_0} \times 100 \quad (4)$$

where: C_0 and C_t represent respectively the liquid phase concentrations of the dye, initial and at the predetermine time intervals (mg.L^{-1}).

It can be observed that the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC provided, in 3h, a percentage of dye removal next to 50%, which confirms the fast filling of its active sites. In addition, within 12h of reaction time, the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC had already removed nearly 100% of the dye (Table 2).

TABLE 2: Methylene blue dye removal percentage at room temperature.

TABELA 2: Percentual de remoção do corante azul de metileno em temperatura ambiente.

Time (h)	Removal (%)
1	36.09
3	49.52
6	86.84
12	99.70
24	99.86

Adsorption isotherm and applied models

Adsorption isotherms are basic requisites for understanding the adsorption process and indicate how the adsorbate is distributed between the liquid and solid phases when the process reaches equilibrium (HAMEED; DIN; AHMAD, 2007; MEZOHEGYI et al., 2012). The isotherm presented in this work was obtained when considering the relation between the equilibrium concentration (C_{eq}) and adsorbate amount adsorbed by the AC (q_{eq}) (Figure 4). It was verified that it presented, initially, an increase in the adsorption, indicating an affinity between the adsorbate/adsorbent, followed by a plateau formation that constitutes the maximum saturation capacity, which happens because of the better adjustment to the Langmuir isotherm (DOTTO et al., 2011).

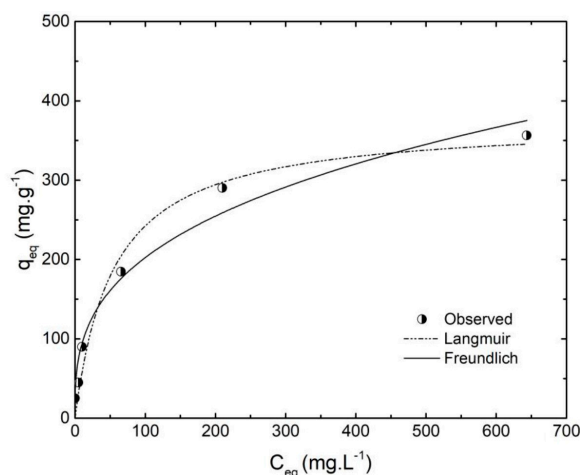


FIGURE 4: Adsorption isotherm for MB (10 mg AC; 10 mL different concentrations solutions; q_{eq} = amount of adsorbed MB; C_{eq} = equilibrium concentration; at room temperature).

FIGURA 4: Isoterma de adsorção para o AM (10 mg de CA; 10 mL de soluções em diferentes concentrações; q_{eq} = quantidade de AM adsorvida; C_{eq} = concentração de equilíbrio; em temperatura ambiente).

The Langmuir and Freundlich models are usually applied in adsorption studies. The Langmuir model, with better adjustment in this work, assumes the formation of a dye monolayer in the surface of AC, in which all of the sites are identical and energetically equivalents, while the Freundlich estimates that the adsorption happens in heterogenic and not specified sites of the AC (BARBOSA et al., 2014).

Langmuir isotherm model

The linearized form of the Langmuir is described according to the Eq. (5) and the Langmuir parameter values, calculated by linear regression, are presented in Table 3.

$$\frac{C_{eq}}{q_{eq}} = \frac{1}{q_m \times K_L} + \frac{1}{q_m} \times C_{eq} \quad (5)$$

where: q_{eq} represents the MB adsorbed quantity (mg.g^{-1}) at a given concentration; C_{eq} the concentration of MB after the equilibrium is reached (mg.L^{-1}); and q_m and K_L are the parameters associated to the maximum adsorption capacity of the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC (mg.g^{-1}) and the Langmuir constant (L.mg^{-1}), respectively.

TABLE 3: Adsorption parameters obtained from the data adjustment to the Langmuir and Freundlich isotherm models for the methylene blue dye at room temperature.

TABELA 3: Parâmetros de adsorção obtidos a partir do ajuste dos dados aos modelos de isoterma de Langmuir e de Freundlich para o corante azul de metileno em temperatura ambiente.

Langmuir Parameters		Freundlich parameters	
q_m (mg.g^{-1})	374.755	N	3.021
K_L (L.mg^{-1})	0.018	1/n	0.331
R_L	0.052	$K_F [(\text{mg.L}^{-1})(\text{L.mg}^{-1})^{1/n}]$	43.985
R^2	0.968	R^2	0.955

Where: q_m = maximum adsorption capacity (mg.g^{-1}); K_L = Langmuir constant; R_L = Dimensionless equilibrium parameter; R^2 = Correlation coefficient; $1/n$ = Sorption intensity measure; K_F = Sorption coefficient.

The maximum adsorption capacity (q_m) obtained for the MB dye in this work was 374.75 mg.g⁻¹ and is in accordance to the maximum values presented in the adsorption isotherms (as show in Figure 4). The q_m value allows to evaluate the adsorption capacity by identifying the AC capacity to retain a certain solute, which can be used to estimate the extension of the movement in the liquid phase. Therefore, this parameter can be understood as a measure of the equilibrium distribution between the solid and liquid phases; the higher the adsorptive capacity of the AC, the higher the obtained q_m value (BORGES et al., 2016). The favorable nature of adsorption could be expressed in terms of a dimensionless equilibrium parameter, R_L , according to the Eq. (6) and the expressed value of R_L can be of an irreversible nature ($R_L = 0$), favorable ($0 < R_L < 1$), linear ($R_L = 1$) or unfavorable ($R_L > 1$) (ABBAS; KADDOUR; TRARI, 2014).

$$R_L = \frac{1}{1 + K_L \times C_0} \quad (6)$$

where: K_L is the Langmuir constant and C_0 the initial dye concentration in the higher analyzed one.

Thus, the obtained R_L value was 0.052, which proves that the adsorption process of the methylene blue dye by the H₃PO₄/H₂O AC was of a favorable nature.

Freundlich isotherm model

The linearized form of the Freundlich isotherm model is described according to the Eq. (7) and the calculated values of the Freundlich presented in Table 3.

$$\log q_{eq} = \log K_F + \frac{1}{n} \log C_{eq} \quad (7)$$

where: q_{eq} represents the amount of adsorbed MB (mg.g⁻¹) at a given concentration; C_{eq} the MB concentration after the equilibrium is reached (mg.L⁻¹); and K_F and $1/n$ are the parameters associated to the H₃PO₄/H₂O AC adsorption parameter [(mg.L⁻¹)(L.mg⁻¹)^{1/n}] and the sorption intensity, respectively (ROCHA et al., 2012).

The adjustment of the observed data to the employed isotherm happened bearing in mind the R^2 values obtained in the Langmuir and Freundlich parameters. Thus, the R^2 values (Table 3) confirm that the Langmuir isotherm model presented a better adjustment to the analyzed data ($R^2 = 0.968$) than the one acquired by Freundlich model ($R^2 = 0.955$). This scenario shows that the adsorption happened in homogeneous and specific active sites of H₃PO₄/H₂O AC, indicating that the adsorption was of a chemical nature (DOTTO et al., 2011).

The n exponent accuses if the isotherm is favorable or unfavorable related to the Freundlich model, with the value of n , in the 1 to 10 interval, expressive of favorable adsorption conditions, which are also related to the scale of adsorbate/adsorbent iteration (ROCHA et al., 2012). The n reached value was 3.021 (Table 3), which shows that the method analyzed for the MB dye was of a favorable nature. However, it can be noticed that the R^2 value was 0.955, proving that the Langmuir model worked better to the data highlighted in this study.

Fraction of dye accessible porosity

The surface area estimated from the adsorption of the MB dye was calculated according to the Eq. (8) and the obtained value was $723.28 \text{ m}^2 \cdot \text{g}^{-1}$. The $S_{\text{MB}}/S_{\text{BET}}$ relation is an indication of the accessible porosity fraction to the MB dye (BRUM et al., 2008). In this study, the relation was 0.53, which indicates that the MB molecules occupy near to 53% of the total porosity found to the S_{BET} of the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC.

$$S_{\text{MB}} = 1000 \times S_{\text{MB}}^{\circ} \times q_{\text{m}} \quad (8)$$

where: S_{MB} = surface area estimated by the MB index ($\text{m}^2 \cdot \text{g}^{-1}$); S_{MB}° = surface area of the MB dye ($S_{\text{MB}}^{\circ} = 1.93 \text{ m}^2 \cdot \text{g}^{-1}$); and q_{m} = maximum MB adsorbed capacity ($\text{mg} \cdot \text{g}^{-1}$) obtained by the produced AC.

Adsorption of methylene blue dye obtained for other adsorbents

The adsorption using AC is an efficient and economic process (ABBAS; KADDOUR; TRARI, 2014). The maximum adsorption capacity, q_{m} , obtained for the methylene blue by the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC, in comparison to other available adsorbents in the literature, are demonstrated in the Table 4.

TABLE 4: Maximum adsorption capacity (q_{m}) of methylene blue obtained for various adsorbents.
TABELA 4: Capacidade máxima de adsorção (q_{m}) do azul de metileno obtida por vários adsorventes.

Raw material	Activating agent	m/m	q_{m} ($\text{mg} \cdot \text{g}^{-1}$)	Reference
Bamboo	$\text{H}_3\text{PO}_4/\text{H}_2\text{O}$	2:1	374.75	This work
Bamboo	KOH/CO_2	1:1	454.20	Hameed et al. (2007)
Rattan	NaOH	-	359.00	Islam et al (2017)
Piassava	ZnCl_2	1:1	276.40	Avelar et al. (2010)
Buriti	ZnCl_2	1:3	274.62	Pezoti Jr et al. (2014)
Piassava	H_3PO_4	1:1	239.12	Avelar et al. (2010)
Cocoa	CO_2	-	212.77	Ahmad et al. (2012)
Coffee	ZnCl_2	1:1	188.70	Brum et al. (2008)
Eucalyptus sp.	K_2CO_3	1:1	81.00	Couto et al. (2012)
Candeia	CO_2	-	16.10	Borges et al. (2016)

Where: m/m = proportion of raw material used (g) / activating chemical agent (g).

Literature shows that the value of q_{m} at essays of adsorption equilibrium for MB dye by various adsorbents can vary from 16.10 to $454.20 \text{ mg} \cdot \text{g}^{-1}$. Thus, it can be said that the $\text{H}_3\text{PO}_4/\text{H}_2\text{O}$ AC can be an excellent adsorbent for dye adsorbing in an aqueous medium, which has been an environment problem. Also, as already described, this result is related to the relatively high value obtained in the S_{BET} analysis (see Table 1) that has great influence with the q_{m} elevation.

According to Abbas, Kaddour and Trari (2014), the differences in the adsorption values are related to the proprieties of each adsorbent, like structure, functional groups and porosity. In addition to those, Mezohegyi et al. (2012) notes several other factors that includes the interaction between the adsorbate and adsorbent, the surface chemical, the dye molecule characteristics, pH, temperature and contact time.

The comparison of the obtained q_m value of synthetized AC with other adsorbents show that its economic and industrial interest (ABBAS; KADDOUR; TRARI, 2014), mainly when considering the amount of chemical activating agent used in the process was cut in half for this study ($m/m = 2:1$).

CONCLUSIONS

The quality and certainly low cost AC production was demonstrated in this study using the bamboo as a raw material. The H_3PO_4/H_2O AC presented a considerably elevated S_{BET} when compared to the S_{BET} values presented in the literature that varies on the 296.01 to 1896.00 $m^2.g^{-1}$ range.

The produced AC was efficient in removing the methylene blue dye, presenting a quick adsorption and high adsorption capacity (374.75 $mg.g^{-1}$). The results obtained in this study recommend the use of the AC H_3PO_4/H_2O in the treatment of the water contaminated by methylene blue dye, foremost in higher concentrations than limits admitted by the legislation.

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