

# Effect of sulphur species on the hydrocarbon biodegradation of oil sludge generated by a gas processing facility

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**Abstract** Oily sludge from gas processing facilities contains components that are major environmental pollutants. Biodegradation is an alternative treatment, but can be affected by other components of the sludge, such as sulphur compounds, so it is important to evaluate the effect of these on oil biodegradation in order to prevent negative impacts. This work studied the transformation of sulphur compounds in oily sludge biodegradation systems at the microcosm level. The predominant sulphur compounds in the original sludge were elemental sulphur and pyrite (9,776 and 28,705.4 mg kg<sup>-1</sup>, respectively). In the biodegradability assays, hydrocarbon concentrations decreased from 312,705.6 to 186,760.3 mg kg<sup>-1</sup> after 15 days of treatment. After this time, hydrocarbon degrading activity stopped, corresponding with a decrease in hydrocarbon degrading bacteria. These changes were related to a reduction in pH that inhibits biodegradation. During the assay, sulphur compounds were gradually oxidized and transformed. The concentration of sulphate increased from 5,096 to 64,868.3 mg kg<sup>-1</sup> after 30 days in the assay, although controls were unchanged. Therefore, it is important to determine changes to the main compounds of the waste in order to assess their impact.

**Keywords** Hydrocarbon biodegradation · Sulphate · Elemental sulphur · Pyrite

## Introduction

Gas processing facilities generate oil sludges, which are oil wastes from purges and separation equipment (Manning and Thompson 1995). The composition of these wastes is variable but overall they contain hydrocarbons and sulphur (EPA 2000). Because it is a heterogeneous matrix of complex components, the handling and disposal of oily sludge is a serious environmental problem (Ward et al. 2003). An alternative treatment for these sludges is biological processing. The effectiveness of this method has been previously demonstrated in the biodegradation of oil sludge from different origins (Bengtsson et al. 1998; Ward et al. 2003), in which removal of 80–99 % of sludge over 60–120 days was achieved with total petroleum hydrocarbon (TPH) concentrations of 26,000–50,000 mg kg<sup>-1</sup>. Other studies report the use of composting biopiles in removal of hydrocarbon from drilling mud and refinery oil sludge with TPH concentrations of 100,000–371,000 mg kg<sup>-1</sup> and removal efficiencies of 31–53 % (Al-Daher et al. 2001; Ouyang et al. 2005; Marín et al. 2006). The difficulty associated with the treatment of oily sludge containing hydrocarbons is that they comprise a mixture of compounds, which may be saturated, aromatic and heteroatom compounds containing sulphur, oxygen or nitrogen (Balba et al. 1998). After carbon and hydrogen, sulphur is the most abundant element in crude oil, in which its concentration can vary from 0.05 to 5 %, but can be up to 14 % in heavier oil (Bahuguna et al. 2011). In reservoirs, sulphur can be found in inorganic forms such as hydrogen sulphide (H<sub>2</sub>S), pyrite (FeS<sub>2</sub>) and elemental sulphur S<sup>0</sup>, or organic compounds such as aromatic and saturated forms of thiols, sulphides and heterocycles (Shennan, 1996). Some of these compounds, such as dibenzothio-  
phene (DBT) and its derivatives, are considered highly

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recalcitrant in sulphur removal processes (Soleimani et al. 2007).

Studies on the presence of sulphur compounds and hydrocarbon biodegradation have focused on the biodesulphurization of thiophene, dibenzothiophene and its derivatives (Shennan 1996; Bressler et al. 1998). In the case of inorganic sulphur (pyrite and elemental sulphur), studies have been directed towards metal leaching (Bacelar-Nicolau and Johnson 1999; Rawlings 2004), and very few have assessed the impact of pyrite in the bioremediation of organic compounds (Sarioglu and Coptý 2008).

The application of biological alternatives for the treatment oily sludge has been aimed at the removal of hydrocarbons (Ouyang et al. 2005; Marín et al. 2006). In most of these studies, no account has been taken of the effect of the presence of other pollutants on degradation, such as sulphur and compounds derived from secondary biological processes that can occur in parallel. These compounds can inhibit the activity of hydrocarbon degraders (Meyer and Steinhart 2000). Therefore, it is important to study changes in sulphurous species and their effect on biodegradation.

The aim of this work was to evaluate the effect of sulphur species on hydrocarbon biodegradation in oily sludge from a gas processing facility. The research described in this paper was performed in laboratories of Instituto Mexicano del Petróleo, Mexico City in 2010.

## Materials and methods

### Sludge sample

Oil sludge was generated in a natural gas processing facility located in Tabasco, Mexico. The oil sludge sample was obtained from an open pool where the wastes were deposited. The sludge sample was placed in plastic containers, transported and stored at 4 °C until its characterization and use.

### Biodegradability assays

Aerobic biodegradation assays were performed as follows: 15 g of oil sludge at 70 % moisture were placed in 125 ml serum bottles, and nitrogen (N) and phosphorus (P) were added as  $\text{NH}_4\text{Cl}$  and  $\text{K}_2\text{HPO}_4$  in order to biostimulate the native microbiota. Bottles were sealed with acrylonitrile rubber stoppers and aluminium seals and incubated at 30 °C at 100 rpm in an orbital shaker (New Brunswick Scientific, model C-25) for a 30 day period. The systems were opened under sterile conditions once

per day for 30 min to ensure an adequate oxygen supply. Samples were measured at the beginning of the experiment and at 15 and 30 days. Six bottles were prepared for each assay (*M1*, *M2* and *M3*) with C/N ratios of 8.3, 14.3 and 33.3 and C/P ratios of 200, 200 and 100, respectively. Two bottles per assay were analysed at each sampling time.

The controls (*C0*) were prepared without the addition of nitrogen and phosphorus and were sterilized by autoclaving. During sampling, an entire bottle of each treatment was taken, and the total content was measured for analysis. Moisture content, pH, heterotrophic and hydrocarbon degrading bacteria, TPH content, sulphur, sulphates and pyrite were quantified in the sludge.

### Analytical methods

Enumeration of heterotrophic bacteria (HB) and hydrocarbon degrading bacteria (HDB) was performed in selective media, by means of the plate-count method, according to Fernández et al. (2006). To determine TPH, sludge samples (1 g) were taken from each bottle and extracted following a modified shaking/centrifugation method using dichloromethane (Arce et al. 2004). The organic extracts were free asphaltene, purified by hexane precipitation. Concentrated samples (1 µl) were analysed by FID-gas chromatography (Agilent Technologies, model 6890) under the conditions described by Rojas-Avelizapa et al. (2006), but increasing the duration of the last step (290 °C for 25 min). Helium was used as the carrier gas at a flow rate of 1.4 ml min<sup>-1</sup>. The temperature of the injector and detector was set at 250 °C. Total nitrogen was measured by the Kjendahl method according to Fernández et al. (2006); total sulphur was measured according to ASTM-D1552-08 (2008); soluble sulphate was extracted with distilled water using a fraction of previously dried sludge, and analysis was performed on the supernatant using a capillary ion analyser (Waters Corp.). Elemental sulphur was analysed in a sludge sample according to Bartlett and Skoog (1954). Pyrite analysis was carried out by Mössbauer spectroscopy with a constant acceleration by Wissel instruments, model MRG-500, complemented by X-ray diffraction (Simens, model D-5000) according to Nava et al. (2006).

Analysis of organic sulphur compounds was carried out using a gas chromatograph (HP-6890) with a Sievers 355 Sulphur Chemiluminescence Detector (SCD) (Castorena et al. 2002). Metals were analysed using the EPA-6010C (2007) technique; pH was analysed with a pH meter Cole Parmer, model Accumet AR50, and moisture content was measured according to Fernández et al. (2006). All analyses were carried out twice.



## Results and discussion

### Sludge characterization

Sludge characterization showed high concentrations of TPH (312,705.6 mg kg<sup>-1</sup> dry matter d.m.), iron (60,200 mg kg<sup>-1</sup> d.m.) and total sulphur (26,928.7 mg kg<sup>-1</sup> d.m.), where 36.6 % of total sulphur was as elemental-S, 6.3 % as sulphate-S, 56.6 % as pyrite-S (FeS<sub>2</sub>) and less than 0.5 % was detected as other organic sulphur compounds (Table 1). Figure 1a shows the chromatogram of organic sulphur compounds, with dibenzothiophene as reference standard in a gas-oil sample. The same conditions were used to analyse an organic extract of oily sludge and detected a single organic sulphur compound at a low concentration (Fig. 1b).

Enumerations of heterotrophic and hydrocarbon degrading bacteria in oily sludge confirmed the presence of native microbiota (Table 1), which is indicative of microorganism viability and the biodegradation potential of the system (Bossert and Kosson 1997; Mishra et al. 2001).

### Hydrocarbon removal, pH and moisture behaviour

In the biodegradation systems (M1, M2 and M3), hydrocarbon biodegradation was observed in contrast to the control; however, no significant differences between the systems were detected. In these systems, the TPH content decreased on average by 40.3 % after 30 days of treatment while in the control the decrease was 9.3 % (Fig. 2). Some studies report

the biodegradation of oil sludge with high hydrocarbon content (Ouyang et al. 2005). Marín et al. (2006), using a biopile composting process with the addition of a texturing agent, report a removal efficiency of 60 % over 3 months of treatment in an oily sludge from a refinery with an initial concentration of 250,000–300,000 mg TPH kg<sup>-1</sup> d.m. The estimated removal rate was 2,000 mg TPH kg<sup>-1</sup> d.m. day<sup>-1</sup>. However, neither the metal nor the sulphur content were reported. These elements are known to impact negatively hydrocarbon degradation (Benka-Coker and Ekundayo 1998; Sandrin and Maier 2003).

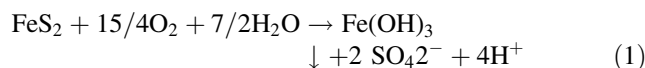
In our study, in addition to high hydrocarbon concentrations, we also found a high metal and sulphur content, which increased the difficulty of the biodegradation process. The initial TPH concentration was 334,700 mg kg<sup>-1</sup> d.m., and the system achieved a removal of 143,921 mg kg<sup>-1</sup> d.m. over 30 days at a rate of 11,156 mg TPH kg<sup>-1</sup> d.m. day<sup>-1</sup>. The TPH removal rate was 5.6-fold higher than that obtained in the work reported by Marín et al. (2006).

In the first 15 days of the biodegradation process, the HB and HDB microbial population increased by about three orders of magnitude (Fig. 3). Between 15 and 30 days, it was observed that TPH degradation was inhibited (Fig. 2), which matched the decrease in HB and HDB bacterial populations (Fig. 3).

The decrease in the bacterial population was related to decreased pH (from 7.9 to 5.3) after 15 days of treatment (Fig. 4a). Kästner et al. (1998) found that, in most cultures, the growth and degradation rates decrease dramatically when the pH drops below 5.0. The maximum values of the hydrocarbon degradation rate and bacterial growth occurred when the initial pH was between 7.5 and 8.5, suggesting that the maximum degradation rate is related to microbial activity (Mutai 2009).

The pH of the control system was unchanged, but decreased in the biodegradation systems; therefore, this change could be attributed to biological factors. It is known that some acidophile microorganisms have the ability to obtain energy from sulphur and iron (Ghauri et al. 2007; Johnson 2009), such as *Thiobacillus ferrooxidans* and *Thiobacillus thiooxidans* species, which can catalyze sulphide or elemental sulphur by oxidation to sulphuric acid (Kuenen et al. 1992; Chazal and Lens 2000).

Other microorganisms, such as *Acidithiobacillus ferrooxidans*, *Acidithiobacillus thiooxidans* and *Gallionella ferruginea*, have the ability to oxidize pyrite (FeS<sub>2</sub>) in the presence of water and oxygen, according to Eq. 1 (Johnson and Hallberg 2005; Chockalingam and Subramanian 2006). The oxidation of elemental sulphur is described in Eq. 2.



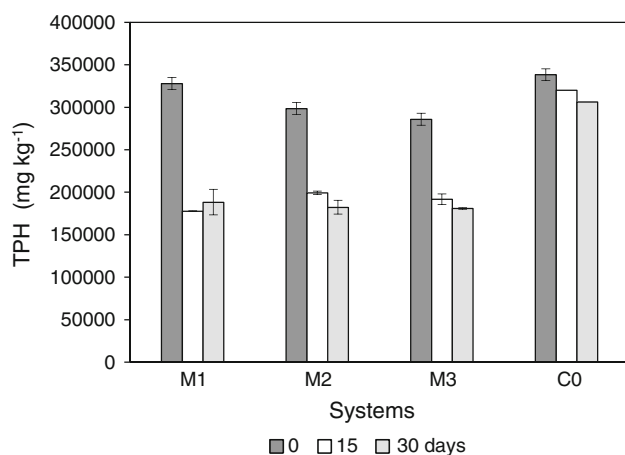
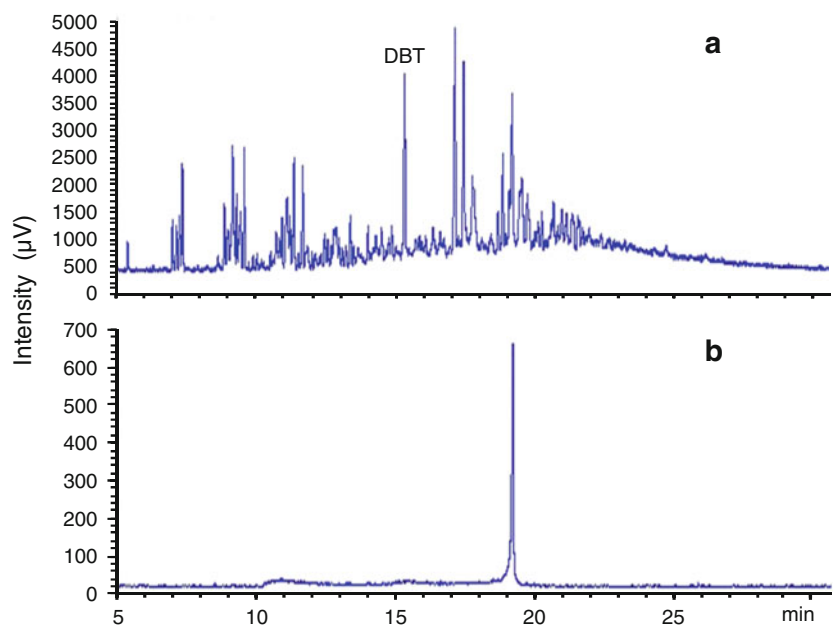
**Table 1** Characterization of oily sludge

Parameter	Concentration
Total petroleum hydrocarbons, TPH (mg kg <sup>-1</sup> d.m.)	334,700 (±7,020)
Total sulphur (mg kg <sup>-1</sup> d.m.)	26,928.7 (±40.4)
Elemental sulphur, S <sup>o</sup> (mg kg <sup>-1</sup> d.m.)	9,776 (±1,147)
Sulphate, SO <sub>4</sub> (mg kg <sup>-1</sup> d.m.)	5,096 (±121)
Iron sulphide, FeS <sub>2</sub> (mg kg <sup>-1</sup> d.m.)	28,705.4 (±2,149)
Organic sulphur compounds (mg kg <sup>-1</sup> d.m.)	124
Organic nitrogen (mg kg <sup>-1</sup> d.m.)	6,275 (±318)
pH	7.82 ± 0.15
Chromium (mg kg <sup>-1</sup> d.m.)	207.28(±8.5)
Zinc (mg kg <sup>-1</sup> d.m.)	8,265 (±110)
Iron (mg kg <sup>-1</sup> d.m.)	60,200 (±179)
Heterotrophic bacteria, HB (CFU g <sup>-1</sup> d.m.)	1.81.1 × 10 <sup>6</sup>
Hydrocarbon degrading bacteria, HDB (CFU g <sup>-1</sup> d.m.)	7.08 × 10 <sup>4</sup>

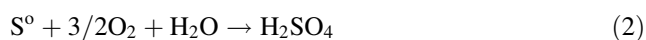
d.m. dry matter



**Fig. 1** GC-SCD chromatograms of organic-sulphur compounds. **a** gas-oil sample, **b** oil sludge. DBT (Dibenzothiophene) was used as reference standard

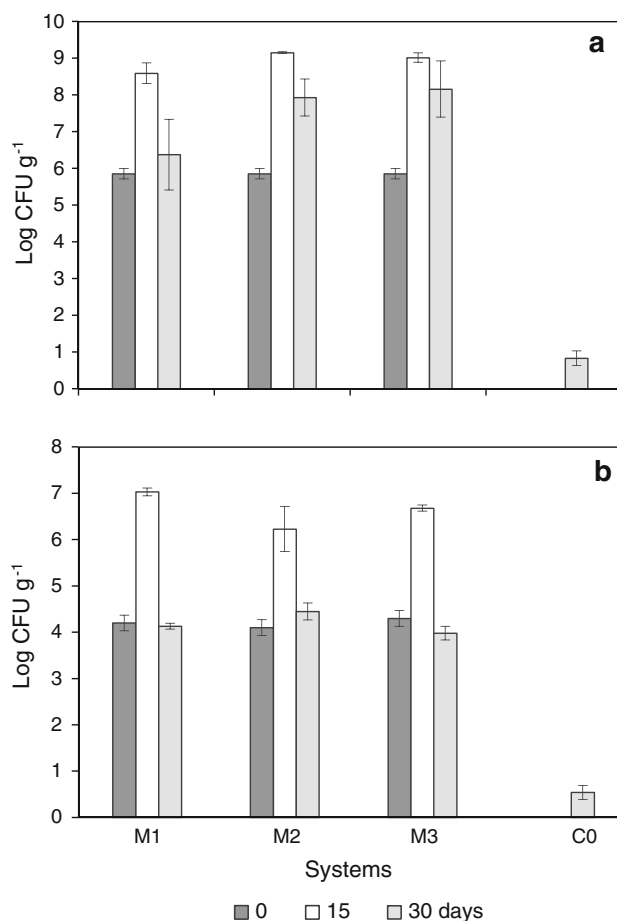


**Fig. 2** HTP content in the biodegradation systems (M1, M2, M3) and sterilized control (C0)



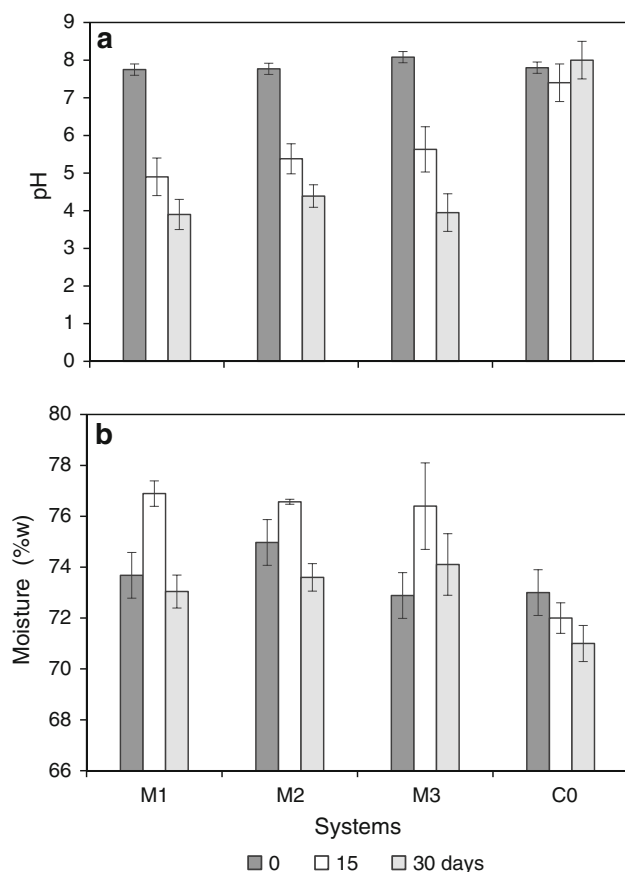
In the conditions of the biodegradation system, the conversion of pyrite and elemental sulphur to sulphate was stimulated by water, aeration and microorganisms. The initial sulphate ( $\text{SO}_4$ ) content of  $5,081 \text{ mg kg}^{-1}$  increased up to  $67,110 \text{ mg kg}^{-1}$  after 30 days of incubation (Fig. 5a), indicative of sulphuric acid ( $\text{H}_2\text{SO}_4$ ) production.

In the biodegradation systems, the moisture content was 73.5 % at the start of the experiment (Fig. 4b). After 15 days, the system recorded an increase in moisture content of 4 % and, at 30 days, this decreased by approximately the same percentage (4 %). This implies that the moisture content was unchanged over the duration of the experiment. Moisture plays an important role because it catalyzes the degradation processes through hydrolysis and



**Fig. 3** Enumeration of bacterial population. **a** Heterotrophic bacteria, **b** Hydrocarbon degrading bacteria, in the biodegradation systems (M1, M2, M3) and sterilized control (C0)



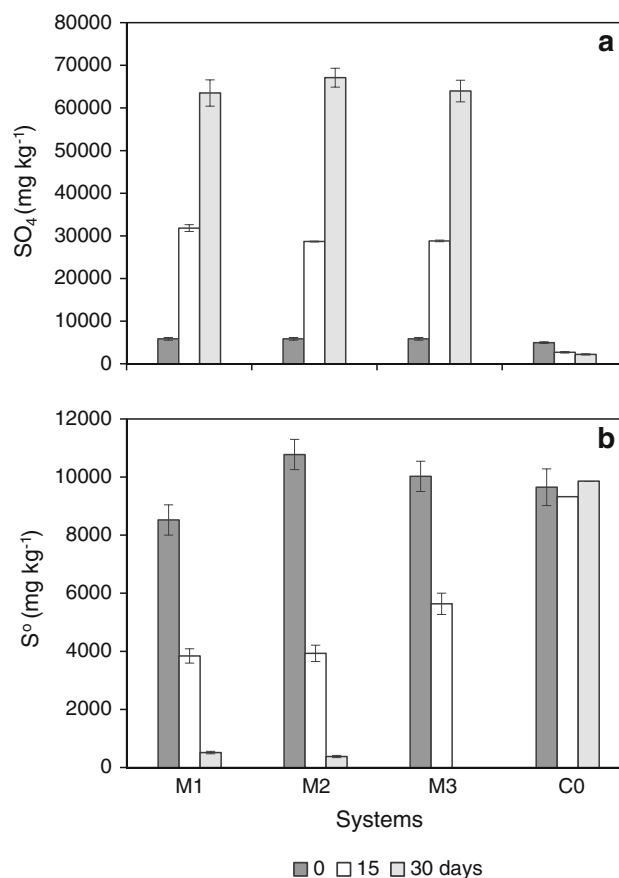


**Fig. 4** Evolution of **a** pH and **b** moisture in the biodegradation systems (M1, M2, M3) and sterilized control (C0)

dissolution of organic and inorganic compounds. The sterile control showed a slight decrease in moisture content.

#### Sulphur balance

Sulphur balance in the systems was based on the quantification of total sulphur, inorganic sulphur species such as sulphate-S, elemental-S<sup>0</sup>, pyrite-S, and organic sulphur compounds-S (osc-S) (Table 2). The initial concentration of elemental sulphur was  $9,776 \pm 1,147 \text{ mg kg}^{-1}$  which decreased by over 50 % after 15 days in the biodegradation systems (Fig. 5b). The inorganic compound with the highest sulphur content in the oily sludge was pyrite (FeS<sub>2</sub>), with a concentration of  $28,705.4 \text{ mg kg}^{-1}$ . At the end of the assay, it was found that the FeS<sub>2</sub> content decreased to  $9,047.7 \pm 1,241 \text{ mg kg}^{-1}$  in the biodegradation systems. The elemental sulphur content decreased by over 96 % of its initial value, and the sulphate-S content increased to  $21,622.7 \pm 651 \text{ mg kg}^{-1}$  (Table 2). This last value is formed by the initial sulphate-S, plus sulphate-S from the elemental-S and pyrite (FeS<sub>2</sub>) oxidation reactions. The final value of sulphate-S was 12.7 times higher than



**Fig. 5** Evolution of **a** Sulphate (SO<sub>4</sub>) production and **b** Consumption of elemental sulphur (S<sup>0</sup>), in the biodegradation systems (M1, M2, M3) and sterilized control (C0)

the value at the start of the experiment. The changes in pH confirmed that the sulphate ion was present as sulphuric acid (H<sub>2</sub>SO<sub>4</sub>). The formation of SO<sub>4</sub> as sulphuric acid from pyrite and elemental sulphur occurs according to Eqs. 1 and 2, respectively. Organic sulphur content in the oily sludge was less than 0.05 %; therefore the contribution of this compound to sulphate production was negligible. The sterile control was unchanged and elemental sulphur content remained at  $9,756.7 \pm 148.9 \text{ mg kg}^{-1}$  over the entire experimental period. The study of sulphur and iron oxidation systems is important for understanding their effect in the biodegradation process of hydrocarbons, in which the oxidation of sulphur to sulphate leads to sulphuric acid production, thus changing the pH of the system and negatively affecting the hydrocarbon degrading activity of microbial groups (Leahy and Colwell 1990; Sarioglu and Copt 2008). Microorganisms that oxidize sulphur under acidic conditions may obtain their energy from sulphur and iron (Kuenen et al. 1992; Chazal and Lens 2000).

Figure 6 shows the correlation between pH and the sulphate concentration described by Eq. 3, with  $r^2 = 0.96$ .



**Table 2** Sulphur species content in biodegradation systems (*M*) and control (C0) before and after 30 days of incubation

	Systems			
	<i>M1</i>	<i>M2</i>	<i>M3</i>	C0
Initial balance				
Elemental-S <sup>o</sup> (mg kg <sup>-1</sup> )	8,524.0	10,778.0	10,026.0	9,651.4
Sulphate-S (mg kg <sup>-1</sup> )	1,680.0	1,745.0	1,671.0	1,694.0
Pyrite-S (mg kg <sup>-1</sup> )	16,582.0	14,328.0	15,080.0	15,454.6
osc-S (mg kg <sup>-1</sup> )	124	124	124	124
Total-S (mg kg <sup>-1</sup> )	26,910.0	26,975.0	26,901.0	26,924.0
Final balance				
Elemental-S <sup>o</sup> (mg kg <sup>-1</sup> )	514.1	377.1	0.0	9,862.0
Sulphate-S (mg kg <sup>-1</sup> )	21,173.1	22,369.6	21,325.6	1,340.0
Pyrite-S (mg kg <sup>-1</sup> )	5,028	4,093.3	5,374.4	15,598.0
osc-S (mg kg <sup>-1</sup> )	124	124	124	124
Total-S (mg kg <sup>-1</sup> )	26,839.2	26,964.0	26,824.0	26,924.0

osc-S: sulphur of organic sulphur compounds

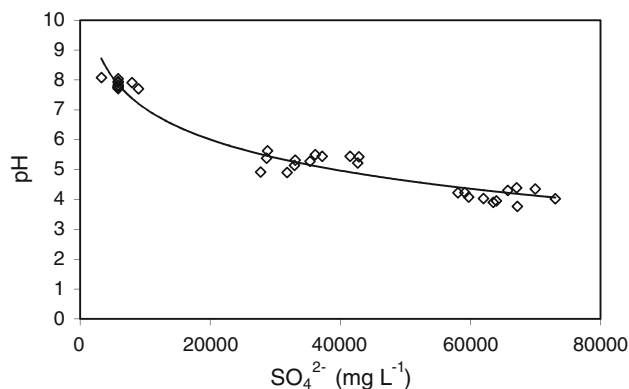
The values are mean of two measures with a variation coefficient (CV) < 10 %

The pH value decreased while the sulphate concentration increased. This indicates that sulphate was present as sulphuric acid (H<sub>2</sub>SO<sub>4</sub>), as has been reported for the metabolism of some sulphur oxidizing microorganisms (Espejo et al. 1988; Sugio et al. 1989; Suzuki et al. 1990).

$$\text{pH} = -1.5\ln(\text{SO}_4 - 2) + 20.86 \quad (3)$$

Biological activity promotes conditions suitable for sulphate production, high acidity and dissolution of metal ions from oily sludge. pH control can mitigate the impact of inorganic sulphur compound oxidation, including pyrite and elemental sulphur, and thus may increase the efficiency of the bioremediation process. The conventional treatment for aqueous systems characterized by high acidity and a high concentration of sulphate and dissolved metal ions is neutralization through the addition of calcium compounds, such as limestone or quicklime, and sodium components, such as caustic soda and soda ash, which result in an increase in pH and precipitation of metal ions. Biological sulphate reduction by sulphate reducing bacteria has also been proposed as an alternative; under anaerobic conditions, the process can remove metals from solution as metal sulphide precipitates (Chockalingam and Subramanian 2006).

Bioremediation processes of organic contaminants containing pyrite have demonstrated that oxygen is a limiting

**Fig. 6** Correlation between pH and sulphate concentrations in biodegradation systems

factor for biodegradation, as most of the oxygen is consumed through ferrous oxidation, while pH also affects the process but can be controlled (Sarioglu and Coptý 2008). This is one of the first studies to analyse the effect of inorganic sulphur compounds on the oil sludge biodegradation process. Although the addition of air and moisture stimulated the activity of HDB, unwanted side effects, such as changes in pH or the dissolution of metals, may result, interfering with remediation (Chockalingam and Subramanian 2006). This work serves to highlight the importance of biodegradation microassays in the detection of problems before the scaling-up of the process for field application.

## Conclusion

The results show that hydrocarbon biodegradation of oil sludge by the native microbiota is feasible. However, the biodegradation process was affected by oxidation of inorganic sulphur compounds that increase sulphate content in the form of sulphuric acid.

In order to eliminate these undesirable effects and to gain better control of the treatment of oil sludge, it is important to monitor changes of sulphur compounds in the hydrocarbon biodegradation process.

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