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Oxidative-reductive photodecomposition of perfluorooctanoic acid in water

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Abstract This article aims to elucidate on usefulness of vacuum ultraviolet (VUV) for photoreductive degradation of perfluorooctanoic acid (PFOA), a representative perfluorinated compound (PFC), in water for the first time. Bench-scale tests were conducted on oxidative and reductive (with aquated electron: e_{aq}^{-}) mineralization of PFOA using low-pressure UV (LPUV) lamps and potassium iodide. Unlike with 254 nm wavelength (UVC), the reductive mineralization with VUV was very inefficient compared to the corresponding oxidative mineralization. The inefficiency is attributed to low reactivity of e_{aq}^{-} with PFOA and its fluorinated products than that of 185 nm photons. Direct VUV photolysis of PFOA and its products in reductive reaction conditions was not apparent due to a very big difference in reactivity of 185 and 254 nm photons with iodide. The results demonstrated that highly energetic VUV photons are not suitable for photoreductive degradations of PFCs involving e_{aq}^{-} , but they can be best used for oxidative degradations. These findings should serve as an important reference on VUV usage to decompose refractory micropollutants.

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Introduction

Occurrence of perfluorinated compounds (PFCs) in water environment and their negative impacts on aquatic ecosystem and human health has been a major focal point of researchers and scientists particularly in the industrialized countries for the last several years. Among the PFCs, perfluorooctanoic acid (PFOA) and perfluorooctane sulfonate (PFOS) have received more attentions as the compounds are widely detected particularly in surface water bodies (Saito et al. 2004; Lien et al. 2006). Effluents from wastewater treatment plants (domestic as well as industrial) are pointed out as the major point sources of these compounds to the water bodies (Clara et al. 2008). Moreover, increasing number of published research reports suggests potential negative impacts of PFCs in water environment on aquatic life and human health (Lau et al. 2004; Corsini et al. 2012; Domingo 2012).

The PFCs are very stable against oxidation, while this characteristic is attributed to the highest electronegativity of fluorine atom (\approx 4.0) and very strong C–F bond (\approx 552 kJ/mol). The advanced oxidation techniques (AOTs) also cannot eliminate the compounds in water due to the inability of powerful and non-selective hydroxyl radicals (°OH) to oxidize them. However, ultraviolet (UV) radiation-based oxidation methods are shown to be more promising than other AOTs. Although direct UVC (254 nm) photolytic degradation of PFOA is negligibly small (Chen et al. 2007; Giri et al. 2011), use of chemical oxidants together with UVC can decompose the compound



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more easily (Chen and Zhang 2006; Wang et al. 2008; Cao et al. 2010; Tang et al. 2012). Furthermore, it has been demonstrated during the last few years that vacuum UV (VUV) (185 nm) photolysis is more efficient than other VU-based methods for PFOA degradation (Chen et al. 2007; Giri et al. 2011, 2012). The carbon-carbon bond in carboxyl functional group is cleaved first followed by formation of fluoride ions due to hydrolysis in stepwise manner during UV oxidation of PFOA and other shorter carbon-chain perfluoroalkyl carboxylates as illustrated in the following equations (Chen et al. 2007):

$$C_7F_{15}COOH (PFOA) + h\nu \rightarrow C_7F_{15} \cdot + \cdot COOH$$
 (1)

$$C_7F_{15} \cdot +H_2O \rightarrow C_6F_{13}COOH (PFHpA) + F^-$$
(2)

$$C_6F_{13}COOH (PFHpA) + h\nu \rightarrow C_6F_{13} \cdot + \cdot COOH$$
 (3)

$$C_6F_{13} \cdot +H_2O \rightarrow C_5F_{11}COOH (PFHxA) + F^-$$
 (4)

Recently, photoreductive reaction using UVC and potassium iodide (KI) is shown as an efficient method than direct UVC photolysis for PFOA degradation and defluorination in water (Park et al. 2009; Park 2010; Qu et al. 2010). Reaction between UVC and KI in absence of dissolved oxygen (DO) generates aquated electrons (e_{aq}) (Iglev et al. 2005), which is a powerful reductant $(E_{aq/e}^{\circ} =$ -2.9 V) responsible for the enhanced PFOA degradation and defluorination. Unlike in UV photooxidation, carbonfluorine bonds are cleaved directly by e_{aq}^{-} as nucleophile during photoreductive degradation of PFOA and other shorter carbon-chain perfluoroalkyl carboxylates as illustrated in the following equations (Qu et al. 2010):

$$\mathbf{I}^- + \mathbf{h}\mathbf{v} \to \mathbf{I}^\cdot + \boldsymbol{e}_{\mathrm{aq}}^- \tag{5}$$

$$C_7F_{15}COOH (PFOA) + e_{aq}^- \rightarrow C_7F_{14}HCOOH + F^-$$
 (6)

$$C_7F_{14}HCOOH + e_{aq}^- \rightarrow C_6F_{13}COOH (PFHpA) + F^-$$
 (7)

$$C_6F_{13}COOH (PFHpA) + e_{aq}^- \rightarrow C_6F_{12}HCOOH + F^-$$
 (8)

$$C_6F_{12}HCOOH + e_{aq}^- \rightarrow C_5F_{11}COOH (PFHxA) + F^-$$
 (9)

Nevertheless, usefulness of the method has yet to be fully understood. Furthermore, it is not yet known what would happen with PFOA degradation and defluorination efficiencies if VUV (185 nm) is used in photoreductive reaction conditions. The first-order rate value for photoreductive degradation of PFOA with aquated electrons $(7.3 \times 10^{-3} \text{ min}^{-1}; \text{ Qu et al. 2010})$ and a roughly estimated first-order PFOA photolysis rate value $(10.2 \times 10^{-3} \text{ min}^{-1}; \text{ Giri et al. 2011, 2012})$ with VUV (185 nm) indicate that photoreductive degradation of PFOA with VUV could be significantly slower than its VUV photolysis degradation. However, this point has not yet been experimentally verified. Moreover, it is also not known



whether photolysis and photoreductive reactions can occur simultaneously in reductive reaction conditions using KI when both the wavelengths (254 and 185 nm) from lowpressure UV (LPUV) lamps are transmitted to reaction solution.

This article aims to (1) clarify whether photoreductive degradation of PFOA in water with VUV is really a slow reaction process than its VUV photolysis and (2) assess whether both photolysis and photoreductive reactions occur simultaneously in reductive reaction conditions utilizing KI in presence of both UVC and VUV. Simple laboratory tests were conducted on UV photolytic and photoreductive degradations of PFOA in pure water using two LPUV lamps and KI in the laboratory of New Industrial Research and Development Center, Osaka Sangyo University, Japan, during May to October of 2012.

Materials and methods

Standards and reagents

Perfluorooctanoic acid (PFOA) standard (CAS: 335-67-1, 99 % purity, Fluorochem Ltd.) was supplied by Wako Pure Chemical Industries Ltd., Osaka. PFOA internal standard (¹³C₄-PFOA, catalog No: MPFOA) was obtained from Wellington Laboratories, Canada. Standards for perfluoroheptanoic acid (PFHpA), perfluorohexanoic acid (PFHxA), perfluoropentanoic acid (PFPeA) and perfluorobutanoic acid (PFBA) were obtained from Wellington Laboratories, while those for perfluoropropionic acid (PFPrA) and trifluoroacetic acid (TFA) were supplied by Wako Pure Chemical Industries Ltd. Other necessary chemicals like acetonitrile (LC/MS grade), ammonium formate, KI were also supplied by Wako Pure Chemical Industries Ltd. Stock solution of PFOA (2.42 mmol/L) in ultrapure water was prepared and stored (4-10 °C). A desired volume of dilute PFOA solution (1.96-3.06 µmol/ L) in ultrapure water was prepared for each test using the stock solution.

Irradiation sources and emission intensities

A 20 W LPUV lamp (UVL20PS-6) and a 110 W LPUV lamp (EUV110US-94L) manufactured by SEN Light Corporation were used in the tests. Measured emission intensities of major (254 nm) and minor (185 nm) wavelengths from the two LPUV lamps are shown in Fig. 1. The 185 nm intensities for 20 and 110 W lamps were about 55 and 78 % of the respective 254-nm intensities. The 185 nm intensity for 110 W lamp was about fourfold larger than the corresponding intensity for 20 W lamp. Similarly, the 254- and 185-nm intensities



Fig. 1 Emission intensities of low-pressure UV lamps used in the tests

for 110 W lamp were about 2.9- and 4.1-fold of the corresponding intensities for 20 W lamp. The increase in 185-nm intensity for 110 W lamp is very notable compared to the increase in 254-nm intensity.

Reactor setup and test procedure

A cylindrical glass reactor (ID: 10 cm, H: 20 cm, V: 1.5 L) described earlier (Giri et al. 2011, 2012) was used for batch tests. A tubular double-layered fused silica glass lamp sleeve with continuous water circulation through the space between the layers was used to ensure transmission of 254 nm alone to reaction solution. A tubular single-layered synthetic fused silica glass lamp sleeve was used to ensure maximum transmission of 185 nm in addition to 254 nm transmission to reaction solution. The lamp sleeves were sealed at the top, and nitrogen gas was continuously passed through the space between lamp and lamp sleeve to remove oxygen and for cooling.

About 1.2 and 1.4 L of reaction solution were used for the tests with UVC and VUV, respectively. An appropriate volume of diluted PFOA solution was poured into the reactor. The solution was continuously mixed using a magnetic bar and stirrer (≈ 300 rpm). An appropriate volume of freshly prepared KI solution was added to reaction solution (initial KI concentration = 0.3 mmol/L) for reductive degradation tests. The particular KI concentration used in these tests is based on a very similar test conducted earlier with UVC and KI (Qu et al. 2010). Solution pH and DO in reaction solution were continuously monitored. No solution pH was adjusted in any of the tests. Pure nitrogen gas (99.9 %) was purged into the reaction solution for about 30 min before beginning of the tests for reductive degradation to remove DO, and the purging continued throughout the test period to ensure anoxic

condition. All the tests were carried out for 3 h, and samples were taken at selected time intervals for analysis.

Sample analysis

Perfluorooctanoic acid (PFOA) and other short carbonchain perfluoroalkyl carboxylates in samples were measured using liquid chromatography tandem mass spectrometry (LCMS/MS, Applied Biosystems). Chromatographic separation was carried out using ZORBAX Eclipse XDB-C18 column (2.1 \times 150 mm, 3.5 μ m) with 200 µL/min flow rate. Ammonium formate in ultrapure water (10 mmol/L) (A) and acetonitrile (B) was used as mobile phases. Each measurement lasted for 30 min with gradient flow of the mobile phases and 5-µL sample volume. The eluent gradient started with 90 % of "A" that linearly decreased to 70 % over the first 3 min. Then, it further linearly decreased to 2 % until 20 min, and this was held constant until 25 min. Then, it increased again to 90 % at 25.1 min, held constant until 30 min, and the measurement was terminated. Electrospray ionization (ESI) was the ion source, while multiple reactions monitoring (MRM) method was used for mass scanning. Nitrogen was used as collision and curtain gas (30 psi) and air was used as nebulizer and dryer gas. Ion source voltage and dryer gas temperature were set at -4,500 mV and 400 °C, respectively. The scanned mass numbers for PFOA, PFHpA, PFHxA, PFPeA, PFBA, PFPrA and TFA were 412.9/368.9, 362.8/319.0, 312.8/268.9, 262.8/218.9, 212.9/138.9, 162.9/119.0 and 112.9/68.9, respectively. Similarly, the mass numbers for PFOA internal standard were 416.8/371.9. Each of the compounds was quantified using a corresponding six-point linear calibration curve (0-100 µg/L).

Fluoride ion concentrations in the samples were measured using ion chromatography (ICS-2000, Dionex). A main column [IonPac AS20 (4.0×250 mm, 7.5 µm)] in series with a guard column [IonPac AG20 (4.0×50 mm, 11 µm)] was used in chromatographic separation. Potassium hydroxide (KOH) solution was used as eluent with gradient flow rate of 1.0 mL/min. The column temperature and sample injection volume were 30 °C and 200 µL, respectively, while each of the measurements lasted for 25 min. Each measurement started with 5 mmol/L KOH concentration in eluent and it remained so until 5 min. The concentration then increased linearly to 30 mmol/L from 5 to 15 min, and it again increased linearly to 45 mmol/L from 15 to 25 min ending the measurement. The fluoride ions quantification was based on a five-point calibration curve (0-200 µg/L fluoride). Organic carbon concentrations in the samples were measured using a total organic carbon (TOC) analyzer (TOC-V_{CSH/CSN}, Shimadzu



Corporation, Japan) with high-sensitivity catalyst for low TOC concentrations.

Results and discussion

The PFCs concentrations, removal ratios and rates, and half-life periods mentioned in the following sections refer to water phase only. PFOA removal and defluorination in these tests are best described by the first-order reaction kinetic. Therefore, the first-order reaction rate values for the two processes are used in discussing the results in this section. The terms "UVC" and "VUV" used in this section denote 254-nm wavelength and combined wavelengths (both 254 and 185 nm), respectively. Moreover, the numbers "20" and "110" immediately after "UVC" and "VUV" indicate rated lamp powers. Both photolysis (i.e., photooxidation) and photoreduction tests were conducted with 20 W lamp, while only photooxidation tests were conducted with 110 W lamp.

PFOA removal ratios and rates

Figure 2a illustrates PFOA removal profiles in terms of ratio and concentration for the five tested cases. The removal ratio profiles were very similar to the corresponding removal concentration profiles. The 3-h removal ratio values for UVC20, VUV20 and VUV110 were about 31, 87 and 100 %, respectively. The values for UVC20/KI and VUV20/KI were about 39 and 72 %, respectively. The removal ratio for UVC20/KI was 1.3fold of the value for UVC20. On the other hand, the ratio for VUV20/KI was 0.8-fold of the value for VUV20 for the same reaction period. Unlike with UVC, photoreductive degradation of PFOA with VUV is apparently very inefficient than the corresponding photooxidative degradation. Among the five cases, photooxidation reaction with increased 185 nm UV energy transmission to reaction solution was the most efficient method for PFOA degradation. For instance, 1-h PFOA removal ratio for VUV110 (97 %) was about 1.6-fold of the value for VUV20 (59 %). In terms of first-order PFOA removal rate (Table 1), UVC20/KI was about 10 % more efficient than UVC20, while VUV20/KI was about 38 % less efficient than VUV20 in these tests. The fourfold increase in 185 nm UV energy transmission to reaction solution for VUV110 case (Fig. 1) is distinctly reflected on the first-order PFOA removal rate value and half-life period (Table 1).

The PFOA removal rate for UVC20/KI in this investigation is about 2.6-fold larger than the value



Fig. 2 a PFOA removal and **b** defluorination profiles for photooxidation and photoreduction reactions. The *solid lines* (primary *y*-axis) represent ratios, while the *dotted lines* (secondary *y*-axis) represent concentrations. The average initial PFOA concentrations in these tests varied between 1.96 and 3.06 μ mol/L

reported in Park et al. (2009 and 2010), but it is about twofold smaller than the value reported in Qu et al. (2010). An optimum KI dosage and alkaline solution pH (\approx 9.0) are shown to enhance reductive degradation of PFOA with UVC (Qu et al. 2010). The twofold smaller value in the present case may be attributed to low solution pH (initial value \approx 5.5, no adjustment/buffering done during the tests) and the choice of KI concentration (0.3 mmol/L). The very small PFOA removal efficiency with VUV20/KI compared to that for VUV20 may be explained as follows. The reported PFOA degradation rates for photooxidation (Giri et al. 2011, 2012) and photoreduction reactions with aquated electrons (Qu et al. 2010) are as follows:

$$UV(254 \text{ nm}) + PFOA \rightarrow P(k = 17.4 \times 10^{-2} \text{ h}^{-1}) \quad (10)$$

UV $(254 \text{ nm} + 185 \text{ nm}) + \text{PFOA} \rightarrow \text{P} \ (k = 81.6 \times 10^{-2} \text{ h}^{-1})$ (11)

$$e_{\rm aq}^- + \text{PFOA} \rightarrow \text{P} \ (k = 43.8 \times 10^{-2} \,\text{h}^{-1})$$
 (12)

Table 1 First-order rate values and half-life periods

Test conditions	UVC20	UVC20/KI	VUV20	VUV20/KI	VUV110
PFOA removal					
$k (h^{-1})$	20.2×10^{-2}	22.2×10^{-2}	81.8×10^{-2}	50.4×10^{-2}	357.6×10^{-2}
R^2	0.9835	0.9868	0.9803	0.9928	0.9917
$t_{1/2}$ (h)	3.50	3.12	0.85	1.37	0.19
Defluorination					
$k (h^{-1})$	0.2×10^{-2}	1.2×10^{-2}	14.3×10^{-2}	3.0×10^{-2}	58.8×10^{-2}
R^2	0.9977	0.9952	0.9933	0.9756	0.9958
$t_{1/2}$ (h)	449.26	57.76	5.00	23.10	1.18

where P denotes degradation products. A rough PFOA photooxidation rate value for 185-nm photons alone can be calculated to be 64.2×10^{-2} h⁻¹ from Eqs. (10) and (12), and this value is about 1.5-fold larger than the value for aquated electrons [Eq. (12)]. Also, the PFOA removal rate value for VUV20 case in this investigation is about 1.6-fold larger than the value for VUV20/KI case (Table 1). It is evident from both experimental and calculated rate values that photoreductive degradation of PFOA with 185-nm photons and KI is very inefficient compared to photooxidative degradation with the photons. It appeared that all the available 185-nm photons in the system were utilized for reductive reactions with KI eliminating any possibility of direct photolysis reaction of PFOA and other short carbonchain PFCs with 185-nm photons. But, the effects (if any) of KI dosage and solution pH on photoreductive degradation of PFOA with 185-nm photons are yet to be understood.

Defluorination ratios and rates

Figure 2b shows defluorination profiles in terms of ratio and concentration. The ratio profiles were very similar to the corresponding concentration profiles. Moreover, the defluorination ratio profiles were very similar to PFOA removal ratio profiles (Fig. 2a). However, defluorination ratios were very small than the corresponding PFOA removal ratios. For example, 3-h defluorination ratio values for UVC20, UVC20/KI, VUV20, VUV20/KI and VUV110 were 0.5, 3.5, 20.5, 7.7 and 69.0 %, respectively. The ratio for UVC20/KI was about sevenfold of the value for UVC20, but the ratio for VUV20 was about 2.7-fold of the value for VUV20/KI. In terms of first-order defluorination rate values (Table 1), UVC20/ KI was about sixfold more efficient than UVC20, while VUV20/KI was about 4.7-fold inefficient than VUV20. It is to be noted here that the effects of reductive reaction with aquated electrons are very profound on defluorination than on PFOA removal both with UVC and with VUV. Similar to PFOA removal rate, the fourfold increase in 185-nm intensity for VUV110 case is clearly reflected on the defluorination rate and half-life period.

The uniqueness of photoreductive degradation of PFOA with UVC and KI is greatly enhanced defluorination that is attributed to direct cleavage of C-F bond by aquated electrons (Qu et al. 2010). In this study also, defluorination rate for UVC20/KI increased by sixfold compared to 1.1-fold increase in PFOA removal rate (the values for UVC20 as references). However, defluorination ratio value for UVC20/ KI (3.5 %) was very small compared to the value (≈ 50 %) reported by Qu et al. (2010) for the similar reaction period. The very big discrepancy in these results is attributed to continuous nitrogen gas purging to reaction solution for photoreductive reactions resulting in easy volatilization of short carbon-chain fluorinated intermediates that ultimately escaped out of the reactor. Similar to PFOA removal, the choice of KI dosage and low solution pH is thought to be other reasons for the small defluorination with UVC20/KI. Mainly two factors are thought to be responsible for the very low defluorination with VUV20/KI compared to that with VUV20. Despite a slightly different PFOA defluorination mechanisms with UV photooxidation and reduction reactions, the reason mentioned earlier for PFOA removal [Eqs. (1)-(3)] should be valid for defluorination too. Furthermore, losses of short carbon-chain intermediates in gas phases due to continuous nitrogen gas purging are thought to have significantly decreased water phase defluorination for VUV20/ KI case. Similar to PFOA removal, any effects of KI dosage and solution pH on defluorination for VUV20/KI are yet to be understood. The very big difference in defluorination between VUV20 and VUV20/KI may also be an indication that all of the available 185-nm photons were utilized in generating aquated electrons eliminating any possibility of oxidation reaction with the photons. Understanding reactivity of KI with 254- and 185-nm photons should clarify the point.



Short carbon-chain fluorinated products and mineralization

Concentration profiles of PFOA and its short carbonchain fluorinated intermediates in water phase during PFOA photodecomposition are illustrated in Fig. 3. The Fig. 3a, b shows VUV20/KI and VUV110 cases, respectively. Though six intermediates at significantly large concentrations were observed with VUV110, only PFHpA, PFHxA, PFPeA and PFBA at low concentrations were observed with VUV20/KI. The concentration profiles of intermediates with VUV20 case (not shown) were very similar, but concentrations were considerably larger than those with VUV20/KI. No other short carbonchain fluorinated intermediates than PFHpA and PFHxA at very low concentrations were observed with UVC20 and UVC20/KI cases. Although the total concentrations of PFOA and its short carbon-chain fluorinated products at the end of 3-h reaction for UVC20/KI and VUV110 cases were apparently very similar, the VUV20/KI case was characterized by very slow degradations of PFOA and the products, while the VUV110 case was characterized by very fast degradations of the compounds. Also, in terms of TOC removals for 3-h reactions,



Fig. 3 Concentration profiles of PFOA and its short carbon-chain fluorinated products for a VUV20/KI and b VUV110 cases. The average initial PFOA concentrations in these cases were 3.06 and 2.51 µmol/L, respectively





Fig. 4 Measured TOC concentrations at the beginning and end of 180-min reactions for VUV20/KI and VUV110 cases

VUV20/KI was very inefficient (≈ 7 % removal, Fig. 4) than VUV20, while VUV110 was the most efficient $(\approx 89 \%$ removal, Fig. 4) among the five cases.

Similar to PFOA removal and defluorination, the inefficiency of VUV20/KI compared to that of VUV20 for PFOA photodecomposition was clearly observed in the formation of short carbon-chain fluorinated intermediates and TOC removals although no distinction was observed between UVC20 and UVC20/KI in this regard. Unlike in defluorination, any impact of volatilization of fluorinated intermediates on TOC removal particularly with VUV20/ KI was not apparent possibly due to the very low removal efficiency. The fourfold increase in 185-nm photon energy with VUV110 (Fig. 1) mineralized PFOA almost completely (Fig. 4). The considerably small defluorination (69 %) compared to the corresponding TOC removal (89 %) in this case may partly be attributed to volatilization of short carbon-chain fluorinated intermediates like TFA, PFPrA and PFBA.

UV photolysis of KI with 254- and 185-nm photons

Although formation of aquated electrons due to KI photolysis with 254- and 185-nm photons was confirmed in the 1960s (Jortner et al. 1964), their (i.e., e_{aq}) usefulness in reductive degradation of PFCs was recognized recently (Huang et al. 2007; Park et al. 2009; Park 2010; Ou et al. 2010). Similar to those results, the UVC20/KI process was more efficient than UVC20 in terms of PFOA elimination and defluorination in this investigation. The process efficiencies should greatly be enhanced further at elevated pH (>9.0) with an optimum KI concentration (if any) for the tested conditions (Qu et al. 2010). Unlike with UVC20/KI, VUV20/KI was very

inefficient than VUV20 in terms of PFOA removal, defluorination and short carbon-chain fluorinated intermediates in this investigation as suggested by PFOA photolysis rate with 185-nm photons and PFOA degradation rate with e_{aq}^{-} [Eqs. (1)–(3)]. Moreover, simultaneous occurrence of photolytic degradation of PFOA by 185-nm photons and PFOA degradation by e_{aq}^{-} in presence of both 185- and 254-nm photons in reductive reaction conditions with KI was not apparent. In this scenario, photolytic reactivity of KI with the two wavelengths should provide clear insight. Jortner et al. (1964) reported large (3.3-fold) quantum yield of e_{aq}^{-} formation with 185-nm photons than with 254-nm photons in iodide solution. This may be taken as clear evidence that the available 185-nm photon energy was used for the formation of e_{aq}^- in VUV20/KI eliminating any possibility of photolysis reaction with the photons ultimately resulting in decreased PFOA mineralization efficiency. Any impacts of solution pH and KI concentration in the reactions are yet to be understood. Nevertheless, determination of KI reactivity with 185- and 254-nm photons using today's experimental facilities should be an option for more insight.

Conclusion

Unlike with UVC, photoreductive mineralization of PFOA in water with VUV was very inefficient than the corresponding photooxidative mineralization, which is attributed to considerably low reactivity of e_{aq}^- with PFOA and its fluorinated intermediates than that of 185-nm photons. Photolysis of PFOA and other short carbon-chain PFCs with 185-nm photons in reductive reaction conditions was not apparent due to very high reactivity of 185-nm photons with iodide than that of 254-nm photons. The results showed that 185-nm photons can be best utilized in oxidative degradations, not in reductive degradations. This is the first investigation on photoreductive degradation of PFOA with 185-nm photons that will be a useful reference on VUV usage for degradations of refractory micropollutants.

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