

# Synthesis of agar-stabilized nanoscale zero-valent iron particles and removal study of hexavalent chromium

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**Abstract** In this study, agar-stabilized nanoscale zero-valent iron (A-nZVI) was synthesized using a rheological phase reaction method. The structure and morphology of A-nZVI particles were investigated by X-ray powder diffraction, scanning electron microscopy, transmission electron microscopy and Fourier-transform infrared spectrometry. Batch removal experiments showed that the pH value of solution, hexavalent chromium [Cr(VI)]/A-nZVI mass ratio and reaction time have significant effects on the removal of Cr(VI). A 100 % removal of Cr(VI) was achieved when applying 50 mg L<sup>-1</sup> of Cr(VI) at the optimal pH value of 3 and the Cr(VI)/A-nZVI molar ratio of 0.025 with the reaction time of 2 h at room temperature. The removal rates of Cr(VI) were fitted to the modified pseudo-first-order kinetic equations with respect to Cr(VI) concentrations.

**Keywords** Agar-stabilized nanoscale zero-valent iron · Rheological phase reaction · Hexavalent chromium · Removal efficiency

## Introduction

Hexavalent chromium is a heavy metal used in a variety of industrial applications which is highly toxic to humans, animals, plants and microorganisms (Gheju 2011). Chromium contamination of aqueous solution has received increasing attention because of its severe impact on public health. Common hexavalent chromium [Cr(VI)] exposure has several contact pathways such as ingestion, inhalation and derma. Cr(VI) has significant effect on human health such as gastrointestinal, respiratory and immunological systems, which can also cause reproductive and development problems. Therefore, it should be removed from contaminated waters. Its reduction to trivalent chromium can be beneficial because a more mobile and more toxic chromium species is converted to a less mobile and less toxic form. Several treatment technologies have been reported for the removal of Cr(VI), including phytoremediation, microbial remediation, chemical reduction, physical sorption (using ion exchange resin, activated carbon etc.) and membrane filtration (ultra filtration, nanofiltration and reverse osmosis) (Owlad et al. 2009). The use of nanoscale zero-valent iron (nZVI) has gained an increasing interest in remediation of surface water, groundwater and soil contaminated with a wide array of organic (Elliott et al. 2009; O'Carroll et al. 2013) and inorganic heavy metals contaminants (Flury et al. 2009; Franco et al. 2009).

The direct mechanism of Cr(VI) reduction is based on the capacity of nZVI to serve as electron donor. Additionally, ferrous iron released during Cr(VI) reduction by nZVI, as well as molecular hydrogen, atomic active hydrogen and solid minerals containing Fe(II) generated as products of nZVI corrosion, may also contribute to the reduction process. The rate of Cr(VI) reduction vary

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significantly depending on experimental conditions such as nZVI type, dose and pretreatment, pH, water composition, temperature and Cr(VI) concentration.

The high remediation efficiency of nZVI is mainly attributed to its high surface area, high levels of surface defects, high density and decent intrinsic reactivity of surface sites, which make the nanoparticles very reactive in the degradation of contaminants (Singh et al. 2011). Nevertheless, nZVI particles synthesized from traditional methods tend to agglomerate rapidly in water via Van der Waals and magnetic attraction forces, forming particles with diameters ranging from several microns to several millimeters (He and Zhao 2005; He et al. 2007; Alidokht et al. 2011). In addition, conventional nZVI particles can react with the surrounding media (e.g., dissolved oxygen, water and other oxidizing agents), leading to the rapid loss of reactivity (He and Zhao 2005; Choi et al. 2009; Alidokht et al. 2011).

To stabilize the synthesized iron nanoparticles, several methods have been investigated. Anionic hydrophilic carbon (Schrack et al. 2004) and chitosan/silica (Zhu et al. 2006) were successfully employed as supports to inhibit the aggregation of iron nanoparticles. Starch (Alidokht et al. 2011) and carboxymethyl cellulose (He et al. 2007) were used as stabilizers to increase the particle dispersion and to improve reaction performance. Iron nanoparticles were immobilized onto supported polyelectrolyte multilayers to yield evenly distributed nanoparticles of uniform size (1–4 nm) (Huang et al. 2008).

Many methods have been used for the preparation of nZVI, such as chemical vapor deposition, inert gas condensation, pulsed laser ablation, spark discharge generation, sputtering gas-aggregation, thermal decomposition, thermal reduction of oxide compounds, hydrogenation of metallic complexes and aqueous reduction of iron salts (Crane and Scott 2012). The properties of metallic nanoparticles are affected by the composition and microstructure, which are sensitive to the preparation method used in their synthesis process.

The rheological phase reaction is the method for preparing compounds or materials from a solid–liquid rheological mixture. There are many advantages in the rheological phase system, such as efficient utilization of the surface area of solid particles, close and uniform contact between solid particles and fluid, good heat exchange and simple reaction temperature control. It is a novel, simple, and economical and efficient soft chemistry method (Jiang et al. 2007).

Agar is also a low-cost and environmentally friendly macromolecular skeleton compound that has been successfully applied as an effective stabilizer in the preparation of metal nanoparticles such as Ag (Shukla et al. 2012). Agar has good rheological properties (Norziah et al. 2006)

that can efficiently utilize the surface area of solid particles. Agar can interact with iron nanoparticles, making them much more stable (He et al. 2007). This is mainly because iron nanoparticles surface is covered by electrically charged agar layers forming electrostatic repulsion and steric effect between molecules, making nano-scale iron particles separate from each other; hence, the dispersion of nanoscale iron was improved (Legrand et al. 2004).

In this study, agar-stabilized nZVI (A-nZVI) was synthesized by rheological phase reaction method and the performance for the removal of Cr(VI) from aqueous solution was investigated.

## Materials and methods

### Preparation of A-nZVI

The stabilized A-nZVI was synthesized as follows: FeS-O<sub>4</sub>·7H<sub>2</sub>O and KBH<sub>4</sub> were mixed at the molar ratio of 1:3 by grinding in an agate mortar, and then, the solid mixture was added to an agar solution to form a rheological body. The mixture was then transferred into a three-necked round-bottom flask. The reaction was conducted under continuous stirring at room temperature. The solid product was collected by filtration, sequentially washed with deionized water and ethanol and dried under vacuum. All reaction processes were protected with nitrogen.

### Characterization of A-nZVI

The X-ray powder diffraction (XRD) patterns were recorded using a Bruker D8 advance diffract meter (Bruker, Germany) with Cu K $\alpha$  radiation from 5° to 70° at a rate of 0.2°/s. The tube current was 100 mA and the tube voltage is 40 kV. The structure and morphology of A-nZVI particles were investigated by scanning electron microscopy (SEM) on a high-resolution SEM (JEOL-JMS-6700F, Japan) with an acceleration voltage of 10–30 kV. The micromorphology was characterized by transmission electron microscopy (TEM) on a high-resolution TEM (HR-TEM, JEOL JEM-2010, Japan) with an acceleration voltage of 200 kV. Fourier-transform infrared (FT-IR) spectrometry recorded with a Nicolet 5700 (Nicolet, US). The spectra were collected with a resolution of 4 cm<sup>-1</sup> in the range of 4,000–400 cm<sup>-1</sup>.

### Batch removal of Cr(VI)

The removal of Cr(VI) was carried out in batch mode at room temperature and atmospheric pressure. 250-mL conical flasks containing a certain amount of A-nZVI and 100 mL of Cr(VI) solution on a temperature-controlled shaker were stirred at 150 rpm. After a desired time, the



solution was filtered through a 0.22- $\mu\text{m}$  cellulose membrane filter to separate out the solid particles.

The Cr(VI) concentration of filtrate was measured using 1,5-diphenylcarbazide method. First, 0.5 mL  $\text{H}_2\text{SO}_4$  (10 + 1) and 0.1 mL 1,5-diphenylcarbazide were added to 5 mL water sample, respectively. Then, Cr(VI) was measured by using a 722 UV-Vis spectrophotometer at 540 nm. The removal efficiency of Cr(VI) was calculated by Eq. (1),

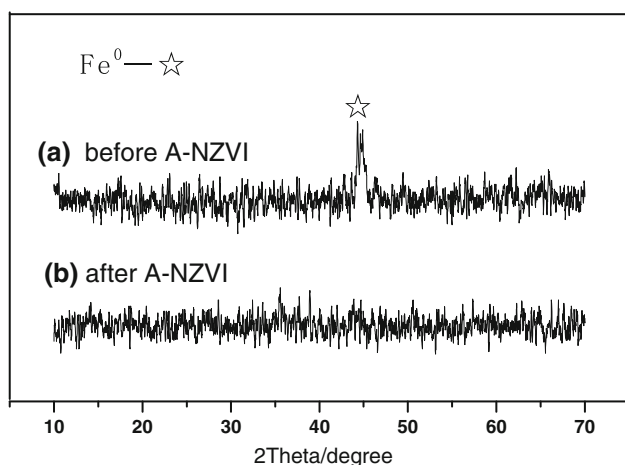
$$E_{\text{removal}} = \frac{(C_0 - C_t)}{C_0} \times 100\% \quad (1)$$

where  $C_0$  and  $C_t$  are the concentrations of Cr(VI) solution at time  $t = 0$  and  $t = t$ , respectively.

## Results and discussion

### XRD analysis

In Fig. 1a, the XRD patterns of A-nZVI after 2 weeks of air exposure indicate the presence of body-centered cubic  $\alpha\text{-Fe}$  (110 and 220) ( $2\theta = 44.83^\circ$  and  $65.22^\circ$ , respectively). In addition, no signal of iron oxides ( $2\theta = 35.46^\circ$ ,  $43.12^\circ$ ,  $53.50^\circ$ ,  $56.98^\circ$ , and  $62.64^\circ$ ) is observed, which indicates A-nZVI has good antioxidant activity. Additional XRD analyses indicate the poor crystalline structure of the nanocluster. Insufficient growth time leads to a tiny nanocluster and poor crystalline structure. After reacting with  $20 \text{ mg L}^{-1}$  Cr(VI) for 120 min, the XRD pattern of A-nZVI changes significantly (Fig. 1b). Cr(III) and iron phases are not detected, which indicates that A-nZVI has changed into amorphous rather than crystalline materials. Research of zero-valent iron and the reduction of chromium shows that the typical result from this deoxidation reaction is chromites,



**Fig. 1** Powder X-ray diffraction patterns of A-nZVI before and after reaction with Cr(VI)

with some of the iron substituted for the chromium. Based on these results, the chromium end product is expected to have the same general chemical formula  $(\text{Cr}_{1-x}\text{Fe}_x)(\text{OH})_3$ , where  $x$  is typically about 0.33. The results obtained by our study are in agreement with that of Ponder et al. (2000).

### SEM and EDX analysis

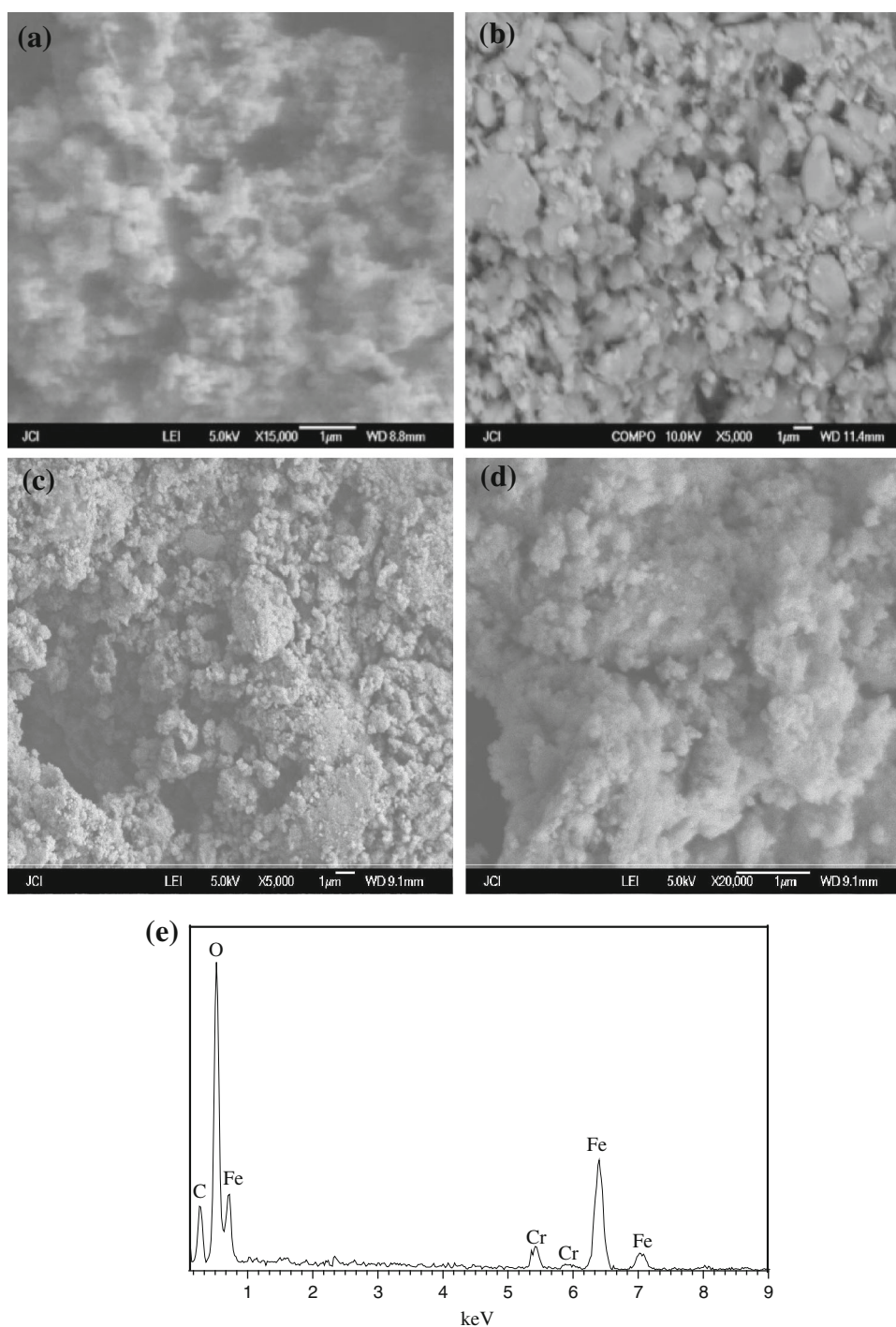
Scanning electron microscopy (SEM) images of freshly synthesized nZVI and A-nZVI are shown in Fig. 2. It can be observed from Fig. 2a that nZVI particles with the diameter of 50–100 nm are in contact with each other. Although they are called “zero-valent iron nanoparticles,” it should be noted that the stack of the aggregated spherical iron particles might be larger than a micrometer rather than existing in separated nanoparticles. This near-linear orientation is due to the magnetic properties of the iron species (Zhang et al. 2006). SEM image of A-nZVI is shown in Fig. 2b. Unlike nZVI, chain-like aggregates of iron nanoparticles can still be observed, as well as the separated iron nanospheres with the diameter of 60–120 nm. These images show that the separation of spherical iron nanoparticles is possible in the presence of an organic dispersing agent (such as agar). Similar results were reported by using carboxymethyl cellulose as the stabilizer (Cirtiu et al. 2011). Figure 2c, d shows the synthesized A-nZVI after reaction. Chain-like iron nanospheres were replaced by flakes/aggregates. This may be attributed to the formation of co-precipitation involving Cr(VI), and the coating of oxide and hydroxide precipitates of Cr(III) and Fe(III) on the surface of the nanoparticles (Ponder et al. 2000). Figure 2e shows energy dispersive X-ray (EDX) spectrum after A-nZVI de-oxidation reaction with Cr(VI) aqueous solution. It shows the O, Cr, Fe and C peak with the weight percent of 54.79 %, 25.13 %, 2.68 % and 17.40 % respectively, in the form of  $\text{Fe}_2\text{O}_3$  and  $(\text{Cr}_{1-x}\text{Fe}_x)(\text{OH})_3$  (Manning et al. 2007). In addition, the carbon would come from agar which can be used to modify nZVI.

### TEM analysis

The distinct iron asthenospheres can be observed clearly in the TEM images of nZVI and A-nZVI as shown in Fig. 3. Figure 3a shows nZVI particles with the diameter of 50–100 nm in contact with each other from a chain-like structure. Spherical asthenospheres are covered by a thin agar layer as shown in Fig. 3b. The different contrast between the center and outer of the spheres indicates the core-shell structure. The nZVI particles are encapsulated into the microspheres by agar and are isolated from each other. For A-nZVI samples, a certain extent of dispersions of nanoparticles is clearly achieved. However, the dispersions are not uniform. The size distribution of nanospheres possesses a wide variation range from 60 to 120 nm



**Fig. 2** **a** SEM image of laboratory made nZVI, **b** A-nZVI, **c** A-nZVI reacted with Cr(VI), **d** A-nZVI reacted with Cr(VI)—  $\times 20,000$  magnifications, **e** EDX element analysis of A-nZVI reacted with Cr(VI)



diameter. Figure 3c, d shows that the surface passivation layers are formed after A-nZVI deoxidation reaction with Cr(VI), due to the precipitation of metal hydroxides on the surface of nZVI.

#### FT-IR analysis

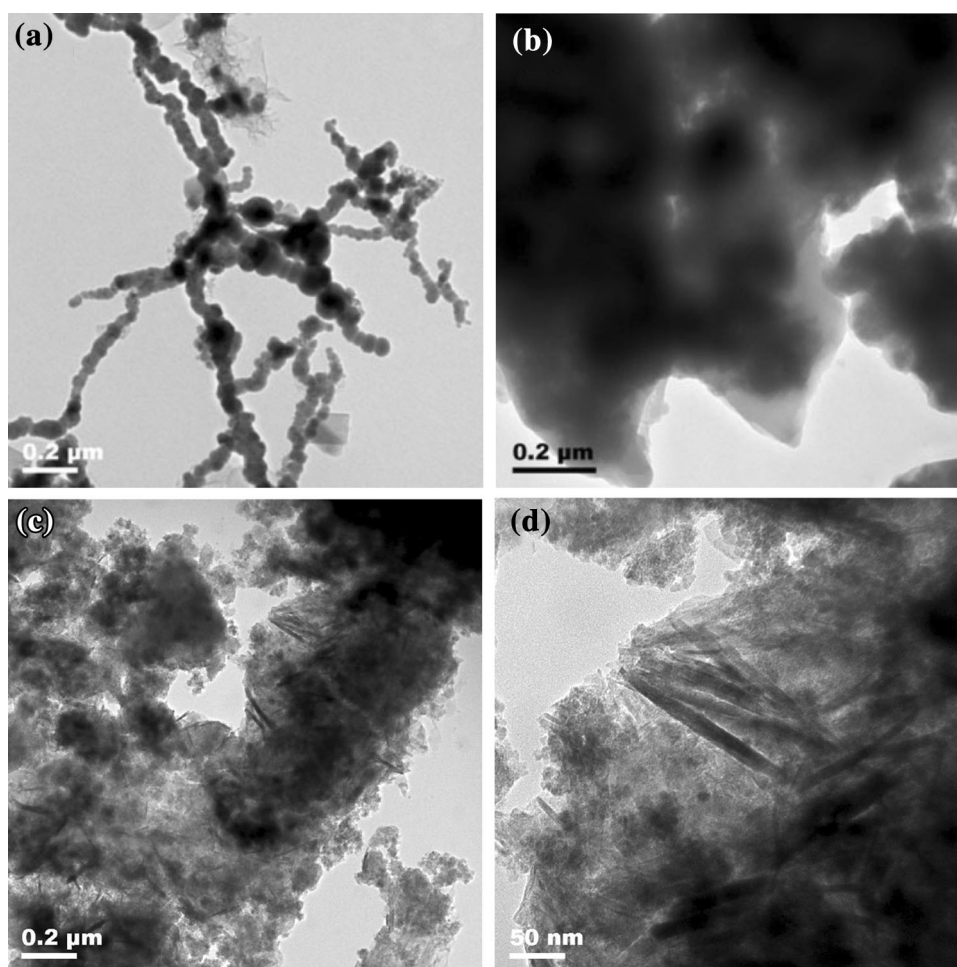
Fourier-transform infrared (FT-IR) spectra of agar and A-nZVI were scanned in the range of  $400\text{--}4,000\text{ cm}^{-1}$  as

shown in Fig. 4. The peak at  $3,400$ ,  $2,900$ ,  $2,360$ ,  $1,650$ ,  $1,360$ ,  $1,160$ ,  $1,080$ ,  $930$  and  $893\text{ cm}^{-1}$  in agar (Fig. 4a) can be attributed to the stretching vibrations of O–H groups. The overlapped bands centered at  $2,900\text{ cm}^{-1}$  are due to the  $-\text{CH}_2$  asymmetric stretches. The peak at  $1,650\text{ cm}^{-1}$ , attributed to agar, is the characteristic absorption band of polysaccharides (Pourjavadi et al. 2009). An intense band between  $800$  and  $1,200\text{ cm}^{-1}$ , corresponding to C–O stretching vibrations, exhibited

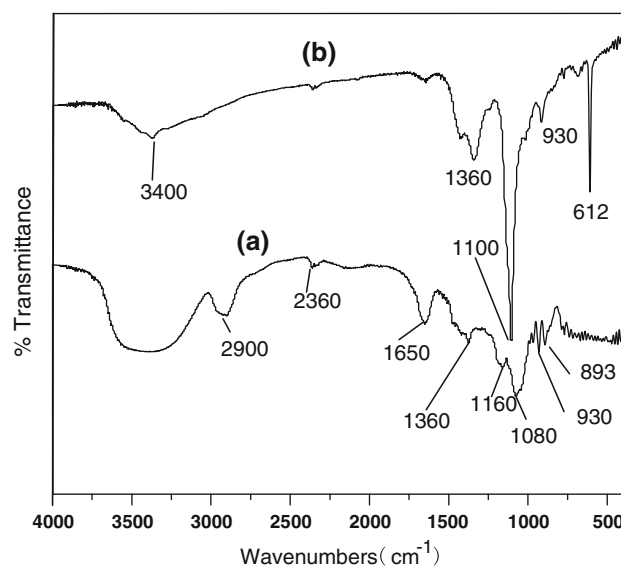




**Fig. 3** TEM image of laboratory made nZVI (a), A-nZVI (b); A-nZVI reacted with Cr(VI) (c); A-nZVI reacted with Cr(VI)—magnifications (d)



peaks centered at 1,160, 930 and 893  $\text{cm}^{-1}$  ( $\nu$  C–O–C) which are assigned to vibrational modes of the glycosidic linkage. The small peak at 930  $\text{cm}^{-1}$  is due to the 3,6-anhydro- $\alpha$ -L-galactopyranose unit. Most of these bands disappeared in the composite, indicating loss of water molecules (Portilla 1976; Zhang et al. 2011). Strong bands at  $<900 \text{ cm}^{-1}$  in the nZVI alone (Fig. 4b), attributable in part to iron oxides on the surface (Zhang et al. 2011; Andrade et al. 2009), are weaker in the composite, indicating less oxidation of agar supported  $\text{Fe}^0$ . The agar support may have reduced Fe (oxy) hydroxide formation, similar to the effect of montmorillonite-supported nZVI (Yuan et al. 2009). Bands at 1,360 and 1,100  $\text{cm}^{-1}$  in the nZVI can be attributed to ethanol used in preparing the sample, but may also include bands associated with sulfate green rust  $[\text{Fe}_4^{\text{II}}\text{Fe}_2^{\text{II}}(\text{OH})_{12}][\text{SO}_4 \cdot 3\text{H}_2\text{O}]$  (Ponder et al. 2001; Gotic and Music 2007) and lepidocrocite ( $\gamma$ - $\text{FeO-OH}$ ) (Andrade et al. 2009) formation on some  $\text{Fe}^0$  surfaces.



**Fig. 4** FT-IR spectra of a agar and b A-nZVI



### The magnetism of A-nZVI

A-nZVI particles can be separated from liquid phase with additional magnetic field. A phenomenon was observed, namely that A-nZVI particle can be evenly dispersed in liquid for 24 h, while bare iron particles are agglomerated and totally precipitate in aqueous solution in 5 min. Therefore, we can see that A-nZVI particle via a rheological phase reaction method has better stability compared with bare iron particles in aqueous solution. In the permanent magnetic field, A-nZVI completely precipitates within 10 min. A-nZVI can be rapidly dispersed in aqueous solution via shaking the conical flask without the magnetic field. The layer of agar on the surface of iron nanoparticles has minor impact on the magnetism of iron nanoparticles. Therefore, A-nZVI can be easily separated from aqueous solution with permanent magnet.

### The removal of Cr(VI) experimental

#### *Influence of A-nZVI dosage and initial concentrations of Cr(VI)*

The influence of A-nZVI dosage on Cr(VI) reduction was examined using the dosages between 0.25 and 1 g L<sup>-1</sup>. The residual Cr(VI) is apparently a function of the applied A-nZVI dose (Fig. 5a): the higher of the A-nZVI concentration, the lower of the residual chromium in solution. A-nZVI concentration of 0.75 g L<sup>-1</sup> can completely reduce Cr(VI) to Cr(III). The increases of nanoparticle concentrations generally increase the number of binding sites, which in turn increase the reduction of Cr(VI). The uptake is a measurement of the amount of Cr(VI) ions bound by unit weight of material. The magnitude decreased with the increasing of the A-nZVI dose.

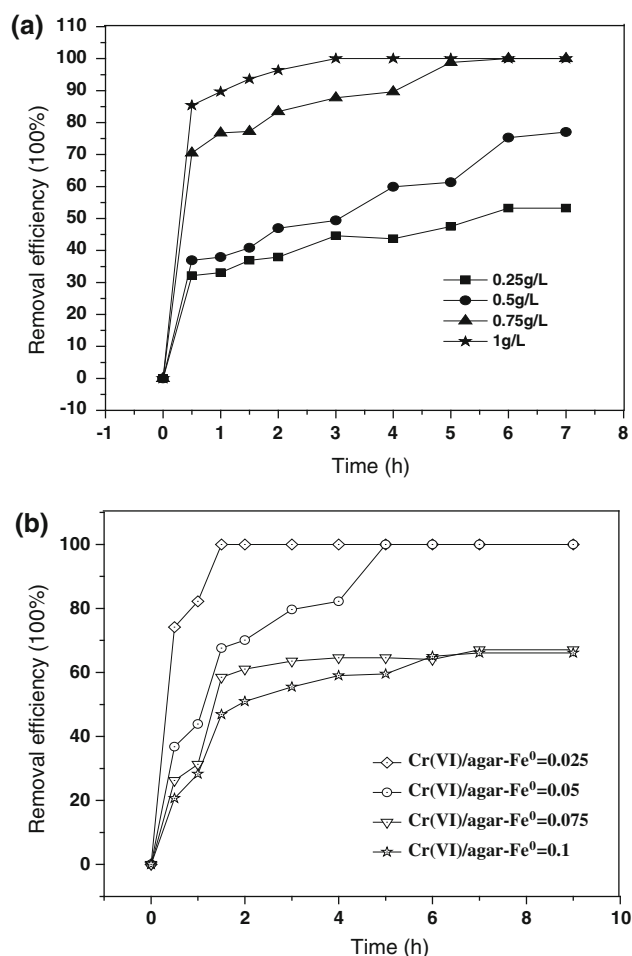
The effect of initial concentrations ranging from 10 to 100 mg L<sup>-1</sup>, pH = 5 and 0.75 g L<sup>-1</sup> A-nZVI at room temperature on the removal of Cr(VI) was discussed. As shown in Fig. 5b, the removal of Cr(VI) decrease with the increase in initial concentration of Cr(VI). Complete removal of Cr(VI) is achieved with the concentrations of Cr(VI) ranging from 10 to 50 mg L<sup>-1</sup>, and 58.05 % of Cr(VI) is removed with the Cr(VI) concentration of 100 mg L<sup>-1</sup> after 5 h of de-oxidation reaction. This might be due to the fact that, for a fixed amount of A-nZVI, the available sites for adsorption remain constant, as the initial concentration of Cr(VI) increasing, the limit activity hinders the de-oxidation reaction leading to low removal of Cr(VI) efficiency.

#### *Effect of pH*

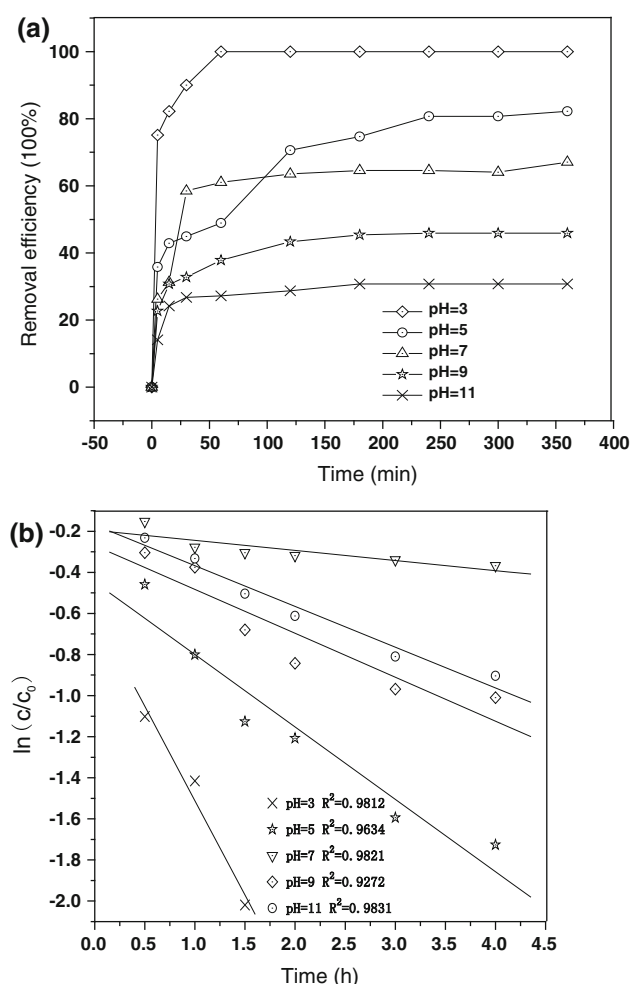
To investigate the effect of pH value on the removal of Cr(VI), batch experiments were carried out with the pH

values ranging from 3.0 to 11.0 with initial Cr(VI) (20 mg L<sup>-1</sup>)/A-nZVI ratios of 0.1 at 25 °C. As shown in Fig. 6a, the removal of Cr(VI) decreases with the increase in the initial pH values from 3.0 to 11.0, and nearly 100 % of Cr(VI) is removed within 60 min at pH = 3. The removal efficiency of Cr(VI) increases with the decrease in pH values, which is because CrO<sub>4</sub><sup>2-</sup>, HCrO<sub>4</sub><sup>-</sup>, H<sub>2</sub>CrO<sub>4</sub>, HCr<sub>2</sub>O<sub>7</sub><sup>-</sup> or Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup> existed on the pH of the medium in the total concentration (Park et al. 2007). In the solutions of low pH values, HCrO<sub>4</sub><sup>-</sup> is the prevalent form of hexavalent chromium, which subsequently shifts to CrO<sub>4</sub><sup>2-</sup> and Cr<sub>2</sub>O<sub>7</sub><sup>2-</sup> as the pH value increases. Low acidic conditions can also cause a high extent of protonated of the nanoparticles surface, resulting in a strong attraction between the negatively charged complex ions and the positively charged surface (Zhang et al. 2011).

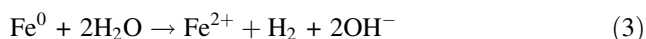
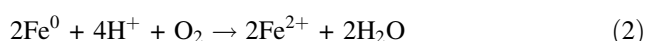
Zero-valent iron (Fe<sup>0</sup>) is a moderate reducing reagent, which can react with dissolved oxygen and to some extent with water (Prabhakaran et al. 2009):



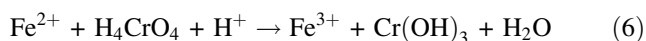
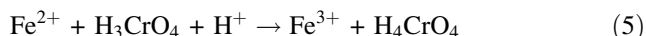
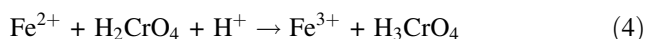
**Fig. 5** Removal of Cr(VI) in the aqueous phase at **a** various A-nZVI dosage and **b** initial concentration as a function of time



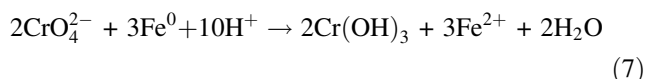
**Fig. 6** **a** Removal of Cr(VI) as a function of time at different pH values. **b** Dynamics curve for treatment of Cr(VI) with A-nZVI on different initial pH



Reduction of Cr(VI) in acidic conditions is described as follows:



To simplify the process, the reaction of Cr(VI) reduced by iron nanoparticles is presented as:



The iron oxidation and reduction reactions are favored at low pH. Moreover, the effect of pH value on the reduction might be influenced not only by  $\text{H}^+$  consumption on the

overall reaction and iron geochemistry but also the relatively low solubility of Cr(III) oxides and mixed Cr(III)/iron (III) oxides (Sass and Rai 1987). When the pH value is higher than 8, only  $\text{CrO}_4^{2-}$  is stable (Weckhuysen et al. 1996).

The influence of initial pH value on the removal rates of Cr(VI) was investigated, and the results are shown in Fig. 6b. For various values of pH from 3.0 to 11.0 with an initial Cr(VI)/A-nZVI ratio of 0.1 at 25 °C, the  $k_{\text{obs}}$  values of the rate constant are 0.9178, 0.2136, 0.1984 and 0.0049  $\text{min}^{-1}$ , respectively. Obviously, plots of  $\ln(c/c_0)$  versus time are linear with a high correlation coefficient ( $R^2 > 0.9$ ) under various conditions (Fig. 6b). This is similar to the results reported in the literature (Shi et al. 2011).

#### Effect of initial Cr(VI)/A-nZVI ratios

Figure 7a shows the effect of initial Cr(VI)/A-nZVI ratios from 0.025 and 0.1 on the removal of Cr(VI) at pH value of 7. The residual concentration of Cr(VI) is a function of the initial Cr(VI)/A-nZVI ratios: the lower of Cr(VI)/A-nZVI ratios, the lower of the residual chromium in solution. As shown in Fig. 7a, the reduction of Cr(VI) increases quickly at the first 2 h, and then, the reduction maintained at a even rate with the increase in reaction time. An initial Cr(VI)/A-nZVI ratio of 0.025 could completely reduce Cr(VI). The increase in the concentration of A-nZVI generally increases the number of binding sites, which in turn increases the reduction amount of Cr(VI).

The reaction of A-nZVI with Cr(VI) belongs to a heterogeneous reaction in aqueous solution. Therefore, the reaction process can be described as Langmuir–Hinshelwood dynamics model (Ho and McKay 1999). These results reveal that the reduction follows a pseudo-first-order kinetic model which can be represented by the following equation:

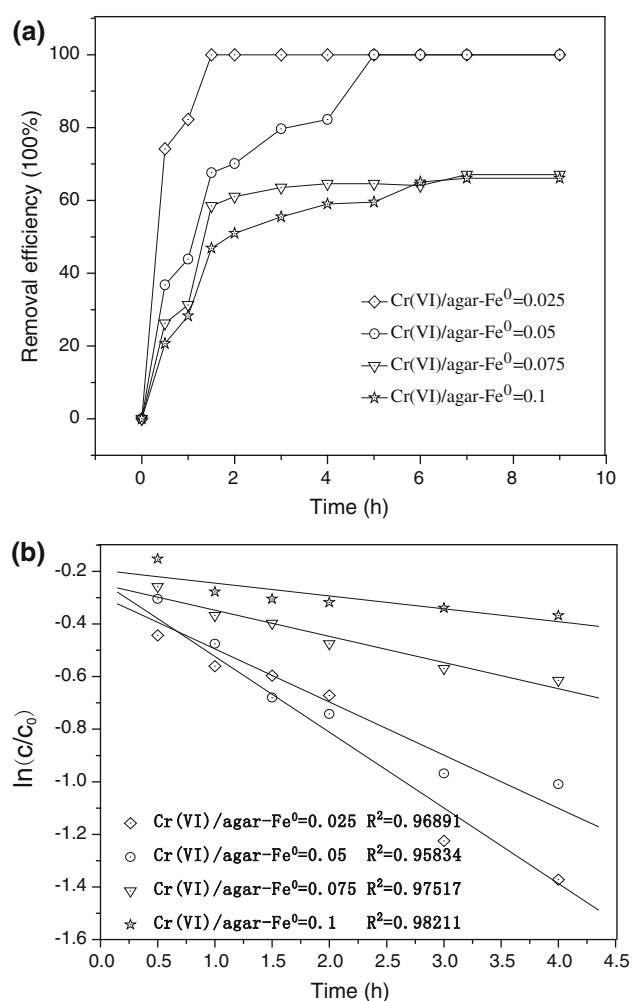
$$v = -\frac{dc}{dt} = K_{\text{SA}} a_s \rho_m c \quad (8)$$

where  $c$  is the concentration ( $\text{mg L}^{-1}$ ) of contaminant in solution,  $k_{\text{SA}}$  is the specific reaction rate constant bounded to the SSA of the materials ( $\text{L h}^{-1} \text{m}^{-2}$ ),  $a_s$  is the specific surface area ( $\text{m}^2 \text{g}^{-1}$ ), and  $\rho_m$  is the mass concentration ( $\text{g L}^{-1}$ ). Since  $k_{\text{SA}}$ ,  $a_s$  and  $\rho_m$  are constant for a given reaction, the product of the three parameters can be replaced by one parameter  $k_{\text{obs}}$ . Then, an evaluation of integrals Eq. (8) can be written as:

$$\ln \frac{c}{c_0} = -K_{\text{obs}} t \quad (9)$$

where  $k_{\text{obs}}$  is the observed rate constant of a pseudo-first-order reaction ( $\text{min}^{-1}$ ) can be determined by the slope of plotting  $\ln(c/c_0)$  versus time.





**Fig. 7** **a** Removal of Cr (VI) as a function of time with different initial Cr (VI)/A-nZVI ratios. **b** Dynamics curve for treatment of Cr(VI) with Agar-Fe<sup>0</sup> on different initial Cr(VI)/A-nZVI ratio

Figure 7b shows the plot of the removal of Cr(VI) by A-nZVI particles using the pseudo-first-order kinetics. The modified first-order model agrees with the kinetics in the whole de-oxidation reaction process. The influence of initial Cr(VI)/A-nZVI ratios on the removal rates of Cr(VI) was investigated. For 100 mL Cr(VI) solution with the initial concentration of 20 mg L<sup>-1</sup> and 0.025–0.1 initial ratios of Cr(VI)/A-nZVI, the  $k_{\text{obs}}$  values of the rate constants are 0.2931, 0.2483, 0.2360 and 0.1950 min<sup>-1</sup>, respectively. The values of observed rate constant ( $k_{\text{obs}}$ ) are obtained with the regression coefficient ( $R^2$ ) around 0.9 (Fig. 7b). Analysis of the data reveals that the rate constants decrease from 0.2931 to 0.1950 min<sup>-1</sup> as the initial ratios of Cr(VI)/A-nZVI increase from 0.025 to 0.1. This can be ascribed to the fact that the specific surface area is constant for a certain material, and the portion of the active sites on the surface of A-nZVI is constant when the portion of iron is fixed. These phenomena could be attributed to an

increasing of the available active sites resulting from the increasing of the A-nZVI dosage. The results obtained are in agreement with previous studies conducted on reaction kinetics (Zhang et al. 2009).

#### Comparison of nZVI and A-nZVI on the removal of Cr(VI)

The initial pH = 5, Cr(VI) concentration was 20 mg L<sup>-1</sup>, and nZVI concentration was 0.75 g L<sup>-1</sup>. It can be seen that, under identical conditions, the removal of Cr(VI) by nZVI and A-nZVI de-oxidation reaction for 5 h were 82.27 and 100.00 %, respectively. This result is supported by the literature (Zhang et al. 2010). The relatively lower removal of Cr(VI) by nZVI was caused by the aggregation of nZVI leading to the decrease in its specific surface area and reaction activity. A-nZVI is a stable material and easy to be dispersed in aqueous solution, and with the presence of agar dissolved, the reaction activity of nZVI increased. In addition, the removal of Cr(VI) by agar is only 3.9 % due to adsorption effect. More importantly, the removal of Cr(VI) by A-nZVI is nearly 100 % after de-oxidation reaction for 5 h, which is much higher than that by nZVI, and even distinctly superior to the simple combination of reduction effect by nZVI and adsorption by agar. For A-nZVI and nZVI, a significant concentration drop in the first 0.5 h is observed. For the control experiment, agar is used for a very small amount of Cr(VI) concentration drop in the first 0.5 h which will help us understand the reduction mechanism. According to the mechanism of the reduction of Cr(VI) (Hoch et al. 2008), the cooperation of agar and nZVI in the agar-nZVI system is favorable for the removal of Cr(VI), and hence, the removal rates of Cr(VI) by agar-nZVI do not decrease comparing to nZVI. The reactivity of entrapped nZVI in calcium alginate beads is comparable to bare nZVI. The results also demonstrate that when the removal of Cr(VI) from solution reached equilibrium in the first 3 h using nZVI, it took 5 h using A-nZVI (Bezbaruah et al. 2009). This indicated that the removal rate of Cr(VI) by nZVI is much faster than that by A-nZVI.

#### The reaction mechanism removing of Cr(VI) by A-nZVI

After the reaction process of Cr(VI) degradation by A-nZVI, A-nZVI evenly dispersed in aqueous solution, the agar layer of iron surface completely dissolved in aqueous solution leads to the Fe<sup>0</sup> exposure to water. The pathway for Cr(VI) removal in aqueous solution is summarized as follows. Removal of Cr(VI) by Fe<sup>0</sup> follows the pathway of sorption and reductive precipitation/immobilization (Lai and Lo 2008; Liu et al. 2008). Initially, Cr(III) adsorbed on the surface of Fe<sup>0</sup> where electron transfer takes place. After sorption, Cr(III) content is reduced with the oxidation of Fe<sup>0</sup> to Fe<sup>2+</sup> and Fe<sup>3+</sup>.



Spectroscopic data showed that the Cr(III) precipitation can form Cr or Cr–Fe mixture such as oxides/hydroxides/oxy-hydroxides (Powell et al. 1995; Pratt et al. 1997). These precipitations were mostly irregular strips, chick-footmark-like or boulder-like forms (Lai and Lo 2008).  $\text{Cr}^{3+}$  and  $\text{Fe}^{3+}$  [ $r(\text{Cr}^{3+}) = 0.615 \text{ \AA}$ ,  $r(\text{Fe}^{3+}) = 0.645 \text{ \AA}$ ] have the similar ionic radii and the valence states;  $\text{Cr}^{3+}$  substitutes  $\text{Fe}^{3+}$  and incorporates into iron oxy-hydroxide shell, forming Cr–Fe mixture such as oxides/hydroxides/oxy-hydroxides with a general chemical formula  $\text{Cr}_x\text{Fe}_{1-x}(\text{OH})_3$ .

## Conclusion

In this study, A-nZVI was synthesized using agar as the stabilizer via a rheological phase reaction method. Batch experiments indicated that A-nZVI had superior removal capability of Cr(VI) in various conditions. The pH value can significantly affect the removal efficiency of Cr(VI). The high removal efficiency of Cr(VI) (100 %) was obtained under the condition of  $50 \text{ mg L}^{-1}$  of Cr(VI) at the optimal pH value of 3 and Cr(VI)/A-nZVI molar ratio of 0.025 for 2 h at room temperature. The removal rate of Cr(VI) was fitted to the modified pseudo-first-order kinetic equation with respect to Cr(VI) concentration.

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